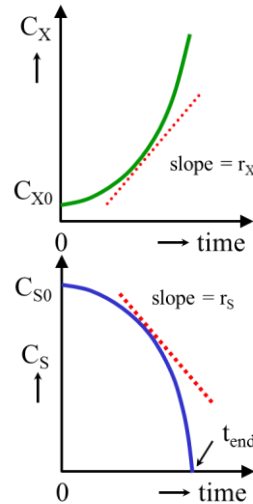


Bioprocesses → Bioreactors

Batch $C_x = C_{x0} \exp(\mu^{\max} t)$

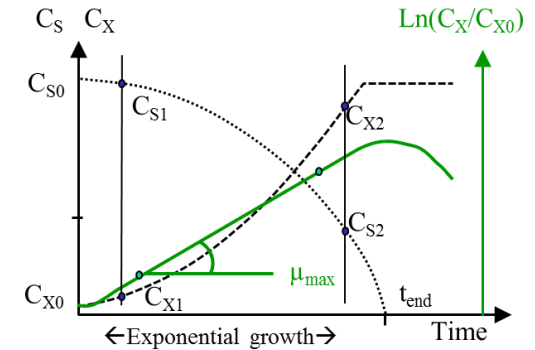
Parameters			state Variables
reactor	operator	micro-organism	
V	C_{S0} C_{X0}	$q_s^{\max}$ $\mu^{\max}$ $Y_{SX}^{\max}$ m_s, K_s	C_S C_X



$$C_{S0} - C_S = \frac{q_s^{\max}}{\mu^{\max}} C_{X0} [\exp(\mu^{\max} t) - 1]$$

$$\mu^{\max} = \text{slope} \ln\left(\frac{C_X}{C_{X0}}\right)$$

$$Y_{SX} \approx Y_{SX}^{\max} = \frac{C_{X2} - C_{X1}}{C_{S1} - C_{S2}}$$

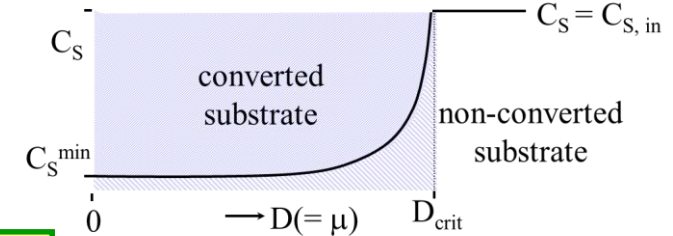


Chemostat

Parameters			state Variables
reactor	operator	micro-organism	
V $\phi_{L,out}$	$\phi_{L,in}$ $C_{S,in}$	$q_s^{\max}$ $\mu^{\max}$ $Y_{SX}^{\max}$ m_s, K_s	C_S C_X

$$C_S = \frac{C_S^{\min} + K_s \frac{D}{\mu^{\max}}}{1 - \frac{D}{\mu^{\max}}}$$

$$C_X = Y_{SX} (\alpha \cdot C_{S,in} - C_S)$$



$$\mu = \frac{r_X}{C_X} = \frac{Q_{L,out}}{V} \stackrel{\text{def}}{=} D : \text{Dilution rate}$$

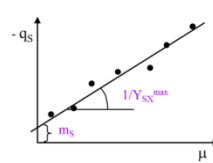
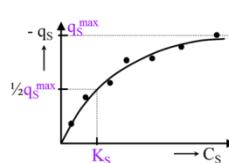
Lineweaver-Burk linearisation

$$\frac{1}{q_s} = \frac{k_s}{q_s^{\max}} \frac{1}{C_S} + \frac{1}{q_s^{\max}}$$

Hanes-Woolf linearisation

$$\frac{C_S}{q_s} = \frac{1}{q_s^{\max}} C_S + \frac{k_s}{q_s^{\max}}$$

Hyperbolic equation $q_s = f(C_S)$



$$D_{\text{crit}} = \mu^{\max} \cdot \frac{(C_{S,in} - C_S^{\min})}{K_s + C_{S,in}} \approx \mu^{\max}$$

