• Outline:

Hydrogen as an energy vector:

- 1. Motivation
- 2. **Properties**
- 3. Production
- 4. Storage
- 5. Distribution
- 6. Application

#### Learning outcomes of todays lecture

- Hydrogen as an energy vector
  - What is hydrogen and what makes it special
  - Why using hydrogen as an energy vector, alternatives
  - How can hydrogen be generated, how renewable
  - How can hydrogen be stored
  - How can hydrogen be transported/distributed
  - Where and how is hydrogen used as an end product

- Current society is largely based on the use of fossil fuels
  - Switzerland: 56% (oil, gas, coal)



• Global: 87% (oil, coal, gas)

• This is not sustainable:

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- Finite reserves (economy)
- Pollution and climate change (environment)
  - Emissions: CO<sub>2</sub>, CH<sub>4</sub>, N<sub>2</sub>O, particles, NO<sub>x</sub>, SO<sub>2</sub>, F-gases, heavy metals (Hg, As)
  - Health issues: smog (winter and summer-smog), ozon layer depletion
  - Climate change: temperature, precipitation,

\*See IPCC report:

snow cover, sea level, etc.\*





• Geopolitical tensions over resources (security)

https://www.ipcc.ch/report/ar5/

• Winter smog in Zürich:





• Summer smog Zürich:





RE, Haussener | April, 2019 5/63

- Increase of renewable energy sources, but issues with
  - Storage
  - Transport, distribution
- Introduction of an energy vector:

An energy vector allows to transfer, in space and time, a quantity of energy.

... energy vectors allow to make energy available for use at a distance of time and space from the source, [independent of] the point of availability of the primary resource in nature.

Orecchini, The era of energy vectors, IJHE, 31, 2006.

- Various energy vectors:
  - Hydrogen
  - Synthetic fuels
  - Fossil fuels
  - Electricity
  - •

#### Table 1 Energy vectors key attitudes

| Energy vector  | Transfer attitude                                     | Storage attitude  |
|--|---|---|
| Fossil fuels   | Short, medium, long range                             | Yes, short, medium, long term.                          |
| Hydrogen   | Short, medium, long range                             | Yes, short, medium, long term.<br>(Cryogenic exception) |
| Heat exchanging fluids                                     | Short range   | Yes, short term   |
| Electricity  | Short and medium range                                | No (indirect methods)                                   |
| Mechanical, oil-dynamic and pressure-dynamic transmissions | Short range   | Yes   |
| Radiation  | Very long range in space<br>Short range in atmosphere | No  |

#### Orecchini, The era of energy vectors, IJHE, 31, 2006.

- Hydrogen has been identified as a possible energy vector and alternative to hydrocarbon-based fuels:
  - Sustainable and environmentally acceptable (produced from water, production/storage/transport can be almost GHG and pollutant free)
  - Independent from crude oil
  - Available from different energy sources
  - Storable in gas, liquid, or metal-hydride form
  - Alternative production technologies
  - Versatile conversion (can be converted in variety of other forms) and application
  - Efficient direct conversion to/from electricity via fuel cells/electrolyzer
  - Almost pollutant free combustion (only NO<sub>x</sub>)
  - Large market potential



• Hydrogen is an energy carrier not an energy source!



Bossel, Does a hydrogen economy make sense?, Proceedings of the IEEE, vol. 94, no. 10, October 2006.

But:

- Charging time of batteries, reliability, range, weight, toxicity •
- Versatility of electricity limited (hydrogen can also be used in ICE, or • as chemical commodity) EPFL RE, Haussener | April, 2019

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- Lightest, most abundant element
  - 90 wt% of the universe
  - 4th most abundant on earth (highly reactive - mainly found in water and hydrocarbons)
- Colorless, odorless, tasteless
- Non-toxic and non-corrosive
- Low viscosity
  (0.89·10<sup>-5</sup> Pa·s @ 293 K, 1 atm)
- Low density
  (0.08345 kg/m<sup>3</sup> @ 293 K, 1 atm)
- Gaseous to 20 K (-253 °C)



• Negative Joule-Thompson coefficient above inversion (inversion 193 K):

$$\mu_{\rm J} = \left(\frac{\partial T}{\partial p}\right)_h$$

• Determined experimentally in an enthalpic expansion process



- Highly diffusive (diffusion coeff.  $0.61 \cdot 10^{-4} \text{ m}^2/\text{s}$ ): rapid mixing
- High solubility: leads to steel embrittlement, enhanced with higher pressure and temperature
- Most energy per unit mass:
  - Hydrogen: 120 MJ/kg
  - Biomass 18 MJ/kg
  - Gasoline 43 MJ/kg



- Safety:
  - Light: rises quickly and disperses
  - High diffusivity: less easy built up of flammable mixtures
  - Small and low viscosity: easily leaks and doesn't accumulate but can also diffuse in metals and embrittle them
  - Small volumetric energy density: holds less energy than gasoline
  - Concentration limits of flammable fuel/air mixture 5-76 vol% (gasoline 1-7 vol%)
  - Autoignition temperature 853 K (gasoline 533 K)
  - Non-toxic
  - Odorless: odorants such as thiole ( R-S, done for natural gas)
     Can be added (already)

• Properties in comparison to other gases and liquids:

| Property   | Hydrogen | Methane | Propane | Gasoline   |
|--|----------|---------|---------|------------|
| Molecular weight (u)   | 2.02     | 16.04   | 44.06   | ~107       |
| Density (kg/m <sup>3</sup> ) at normal conditions                | 0.084    | 0.651   | 1.87    | 4.4        |
| Buoyancy (density with respect to air)                           | 0.07     | 0.55    | 1.52    | 3.4 to 4.0 |
| Diffusion coefficient (cm <sup>2</sup> /s)                       | 0.61     | 0.16    | 0.12    | 0.05       |
| Lean flammability limit in air (% by volume)                     | 4.1      | 5.3     | 2.1     | 1.0        |
| Rich flammability limit in air (% by volume)                     | 75       | 15      | 10      | 7.8        |
| Minimum ignition energy (mJ)                                     | 0.02     | 0.29    | 0.26    | 0.24       |
| Minimum self-ignition energy (K)                                 | 858      | 813     | 760     | 501 to 744 |
| Lean detonability limit in air (% by volume)                     | 18       | 6.3     | 3.1     | 1.1        |
| Rich detonability limit in air (% by volume)                     | 59       | 13.5    | 7.0     | 3.3        |
| Explosion energy (kg equivalent TNT per m <sup>3</sup> of vapor) | 2.02     | 7.02    | 20.2    | 44.2       |

^ Selected physical properties of hydrogen, methane, propane and gasoline.

### Hydrogen use

• Current yearly world production ~55 mio tons and used for:





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|                          | Electrolysis, 1%                           |                                 |                     |
|--------------------------|--|---------------------------------|---------------------|
| • Production of hyd      | rogen:                                     |                                 | Oil, 23%            |
| Technology               |  | <b>F</b>                        | Natural<br>gas, 76% |
| Technology               | Hydrogen source                            | Energy source                   |                     |
| Steam reforming          | Natural gas                                | Combustion, solar               |                     |
| Gasification             | Coal,<br>carbonaceous<br>material, biomass | Combustion, solar               |                     |
| Thermal cracking         | Natural gas, oil                           | Combustion, solar               |                     |
| Thermal dissociation     | Water                                      | Solar                           |                     |
| Thermochemical<br>cycles | Water                                      | Solar, nuclear                  |                     |
| Photoelectrochemical     | Water                                      | Solar                           |                     |
| Electrolysis             | Water                                      | Electricity from rene<br>fossil | ewable, nuclear,    |

• Steam reforming: uses light hydrocarbon feedstock, usually methane, reacts it at elevated temperatures with steam and catalytically converts the feed into hydrogen

 $CH_4 + H_2O \rightarrow CO + 3H_2 (\Delta H = 206 \text{ kJ/mol})$ 



water gas shift:  $CO + H_2O \rightarrow CO_2 + H_2$  ( $\Delta H = -41$  kJ/mol)

Gasification: uses carbonaceous materials, reacts it at high temperatures (>700 °C), without combustion, with a controlled amount of steam, oxygen, and/or CO<sub>2</sub>. Results in CO, H<sub>2</sub>, and  $CO_2$ . 1600 12

$$C + H_2O \rightarrow CO + H_2$$

- Consists of (sequential or simultaneous): Dehydration Pyrolysis (thermal d in the d in the absence of  $O_2$ , devolatilization)
  - Gasification (heterogeneous gas-• solid reaction of pyrolysis residue with reactive gas)
  - Combustion

EPFL

Water-gas-shift



• Thermal cracking: complex organic molecules such as heavy hydrocarbons are broken down into simpler molecules such as light hydrocarbons, by the breaking of carbon-carbon bonds in the precursors at high temperatures and by using catalysts

 $CH_4 \rightarrow C + 2H_2 (\Delta H = 74.85 \text{ kJ/mol})$ 

- Hydrogen derived from fossil fuels has many impurities:
  - From combustion: CO<sub>2</sub>, CO, N<sub>2</sub>
  - From the feedstock: sulfur
- Purification:
  - Desulfurization for gaseous feedstock: calcium-based slurries (SO<sub>2</sub> to sulfites and sulfates)
  - Desulfurization from solid/liquid feedstock: via catalysts into  $H_2S$
  - CO<sub>2</sub> removal:
    - temperature swing adsorption (solubility variation of CO<sub>2</sub> with temperature)
    - pressure swing adsorption (pressure dependent absorption of e.g. zeolites)
    - special membranes (cellulose)
  - CO removal from H<sub>2</sub> mixture: Hydrogen-permeable membranes made of metals (palladium)

- Heat for steam reforming, gasification, or cracking can be produced via:
  - Autothermal processes (partial combustion of the feedstock)

Combustion:  $C_xH_y + (x+y/4)O_2 \rightarrow xCO_2 + y/2H_2O$ 

• Any other heat source such as solar or nuclear:





• Thermal and thermochemical approaches:



• Thermochemical cycles – solar: concentrating technologies



Parabolic through

Solar tower

Fresnel



• Temperatures reachable:

$$\eta_{\rm rec} = \frac{q_{\rm use}}{q_{\rm sol,in}} = \frac{q_{\rm use}}{CI} = \alpha - \sigma \varepsilon \frac{T_{\rm abs}^4 - T_{\rm amb}^4}{CI}$$
$$\eta_{\rm heat-to-electricity} = \frac{T_{\rm abs} - T_{\rm amb}}{T_{\rm abs}}$$



• Thermochemical cycles – nuclear:

- Possible coolants/ heat transfer fluid:
  - Molten-salt
  - Gases (e.g. He)
  - Heavy metals



• Compared to solar: limited in temperature (1573 K)

• Thermal dissociation:

#### $H_2O \rightarrow 1/2O_2 + H_2$



• Multi-step water-splitting cycles

$$H_{2} \xrightarrow{\mathsf{MeO}} H_{2} \xrightarrow{\mathsf{Me+1/2O}_{2}} \xrightarrow{\mathsf{MeO}_{2}} H_{2} \xrightarrow{\mathsf{MeO}_{2}} \xrightarrow{\mathsf{MOO}_{2}} \xrightarrow{$$

- reduce required temperatures
- omit explosive  $H_2/O_2$  mixture



• Possible redox pairs for two-step cycles:

| Cycle   | Reactions  | Cycle                 | Reactions  |
|---|--|-----------------------|--|
| Zn/ZnO  | $ZnO \rightarrow Zn + O_2$   | SoO <sub>2</sub> /SiO | $SiO_2 \rightarrow SiO + 1/2 O_2$                |
|   | $Zn + H_2O \rightarrow ZnO+H_2$  |                       | $SiO+H_2O \rightarrow SiO_2+H_2$                 |
| Fe <sub>3</sub> O <sub>4</sub> /FeO               | $Fe_3O_4 \rightarrow 3 FeO + \frac{1}{2}O_2$   | W/WO <sub>3</sub>     | $WO_3 \rightarrow W+3/2 O_2$                     |
|   | $3 \text{ FeO} + \text{H}_2\text{O} \rightarrow \text{Fe}_3\text{O}_4 + \text{H}_2$                                |                       | $W+3H_2O\rightarrow WO_3+3H_2$                   |
| In <sub>2</sub> O <sub>3</sub> /In <sub>2</sub> O | $In_2O_3 \rightarrow In_2O+1/2 O_2$  | Hg/HgO                | $Hg+H_2O\rightarrow HgO+H_2$                     |
|   | $In_2O+2H_2O\rightarrow In_2O_3+2H_2$  |                       | $HgO\rightarrow Hg+1/2O_2$                       |
| SnO <sub>2</sub> /Sn                              | $SnO_2 \rightarrow Sn+O_2$   | Cd/CdO                | $Cd+H_2O\rightarrow CdO+H_2$                     |
|   | $Sn+2H_2O \rightarrow SnO2+2H_2$   |                       | $CdO \rightarrow Cd+1/2O_2$                      |
| MnO/MnSO <sub>4</sub>                             | $MnSO_4 \rightarrow MnO+SO_2+1/2O_2$   | CO/CO <sub>2</sub>    | $CO+H_2O\rightarrow CO_2+H_2$                    |
|   | $MnO+H_2O+SO_2\rightarrow MnSO_4+H_2$  |                       | $CO_2 \rightarrow CO + 1/2O_2$                   |
| FeO/FeSo <sub>4</sub>                             | $FeSO_4 \rightarrow FeO+SO_2+1/2O_2$   | $Ce_2O_3/CeO_2$       | $CeO_2 \rightarrow Ce_2O_3$                      |
|   | $FeO+H_2O+SO_2\rightarrow FeSO_4+H_2$  |                       | $Ce_2O_3+H_2O\rightarrow 2CeO_2+H_2$             |
| CoO/CoSO4   | $CoSO_4 \rightarrow CoO + SO_2 + 1/2O_2$   | Mg/MgO                | MgO $\rightarrow$ Mg+1/2O <sub>2</sub>           |
|   | $CoO+H_2O+SO_2\rightarrow CoSO_4+H_2$  |                       | $Mg+H_2O\rightarrow MgO+H_2$                     |
| Fe <sub>3</sub> O <sub>4</sub> /FeCl <sub>2</sub> | $Fe_3O_4+6HCl \rightarrow 3FeCl_2+3H_2O+1/2O_2$  | SnO/SnO2              | $SnO_2 \rightarrow SnO+1/2O_2$                   |
|   | $3$ FeCl <sub>2</sub> + $4$ H <sub>2</sub> O $\rightarrow$ Fe <sub>3</sub> O <sub>4</sub> + $6$ HCl+H <sub>2</sub> |                       | $SnO+H_2O\rightarrow SnO_2+H_2$                  |
| Mo/Mo <sub>2</sub>                                | $MoO_2 \rightarrow Mo+O_2$   |                       |  |
|   | $Mo+2H_2O \rightarrow MoO_2+2H_2$  |                       |  |
| the first states                                  |  |                       | <b>RE, Haussener</b>   <b>April</b> , 2019 31/63 |



Oil, 23%

Natural

Electrolysis, 1%

| Technology           | Hydrogen source   | Energy source gas, 76%               |
|----------------------|-------------------|--------------------------------------|
| Steam reforming      | Natural gas       | Combustion, solar                    |
|                      | Coal,             |                                      |
|                      | carbonaceous      |                                      |
| Gasification         | material, biomass | Combustion, solar                    |
| Thermal cracking     | Natural gas, oil  | Combustion, solar                    |
| Thermal dissociation | Water             | Solar                                |
| Thermochemical       |                   |                                      |
| cycles               | Water             | Solar, nuclear                       |
| Photoelectrochemical | Water             | Solar                                |
|                      |                   | Electricity from renewable, nuclear, |
| Electrolysis         | Water             | fossil                               |

**Production** 

electrol vte

H<sup>+</sup>

 $H_20 \rightarrow 2H^+ + 2e^- + 1/20^-$ 

E NHE

-1.0

-0.5

0.0

0.5

absorbe

GaAs

AE =

1.4 eV

 $2H^++2e^- \rightarrow H_2$ 

GaF

 $\Delta E =$ 

2.25 eV

CdSe

 $\Delta E =$ 

 $\Delta E =$ 

2.4 eV

ZnO

 $\Delta E =$ 

3.2 eV

ΔE = 2.1 eV

 $\Delta E =$ 

2.6 eV

ΔE = 3.8 eV

• Photoelectrochemical:

- Stringent material requirements:
  - band gap size
  - suitable band edge position
  - high chemical stability in the dark  $\begin{bmatrix} 1.0 \\ 5 \\ 2.0 \\ 2.$
  - efficient charge transport in the semiconductor
  - selective and efficient electrochemical reactions
  - earth-abundance and low costs

H5/H,

H,O/O.

AE =

3.0 eV

 $\Delta E =$ 

3.2 eV



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Natural

Electrolysis, 1%

| Technology           | Hydrogen source   | Energy source gas, 76%               |
|----------------------|-------------------|--------------------------------------|
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| Thermal dissociation | Water             | Solar                                |
| Thermochemical       |                   |                                      |
| cycles               | Water             | Solar, nuclear                       |
| Photoelectrochemical | Water             | Solar                                |
|                      |                   | Electricity from renewable, nuclear, |
| Electrolvsis         | Water             | fossil                               |

**Production** 

• Electrolysis, e.g. SPE

$$H_2O \rightarrow 1/2O_2 + H_2 ~(\Delta G = 237 \text{ kJ/mol})$$

• At standard conditions (25 °C and 1bar)

$$\Delta G = nFV_{rev} \rightarrow V_{rev} = \Delta G / (nF) = 1.23V$$



• Practical:

$$V = V_{rev} + \eta_a + \left|\eta_c\right| + \eta_\Omega$$

Overpotential due to electrochemical reactions and ohmic losses

$$\eta_{a,c} = a + b \log(i)$$
 Tafel relation

• Alkaline electrolyzer: uses high pH electrolytes (KOH, NaOH) Anode:  $2OH^- \rightarrow \frac{1}{2}O_2 + H_2O + 2e^-$ Cathode:  $2H_2O + 2e^- \rightarrow H_2 + 2OH^-$ 



NEL-Hydrogen: 50-485 Nm<sup>3</sup> H<sub>2</sub>/h 25% KOH aqueous solution, 80°C

• Solid polymer electrolyzer: polymeric electrolyte PEM fuel cell:

Anode:  $H_2O \rightarrow \frac{1}{2}O_2 + 2H^+ + 2e^-$  Cathode:  $2H^+ + 2e^- \rightarrow H_2$ 

、 CF2

- Sulfonated tetrafluoroethylene:
  - Semi-permeable for products
  - Withstand large pressure differentials
  - Proton conducting (10 S/m)
  - Not conducting for electrons
- Membrane is usually only 150-300  $\mu$ m thick
- Commonly uses rare metals as catalysts (Pt, Ir, Ru)
- Gas diffusion layers:
  - Electrical conducting
  - Gas diffusing, permeable
  - Mechanical stable

EPEL





 Solid oxide electrolyzers: operate at very high temperatures (~700-1000 °C)



- Electricity from:
  - Solar: PV electricity
  - Solar: solar thermal electricity
  - Wind
  - Hydro
  - Geothermal
  - Biomass

EPFL

• Fossil fuels







Oil, 23%

Natural

Electrolysis, 1%

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|                      | Coal,             |                                      |
|                      | carbonaceous      |                                      |
| Gasification         | material, biomass | Combustion, solar                    |
| Thermal cracking     | Natural gas, oil  | Combustion, solar                    |
| Thermal dissociation | Water             | Solar                                |
| Thermochemical       |                   |                                      |
| cycles               | Water             | Solar, nuclear                       |
| Photoelectrochemical | Water             | Solar                                |
|                      |                   | Electricity from renewable, nuclear, |
| Electrolysis         | Water             | fossil                               |

**Production** 

• Prize comparison:

| TechnologyPrimary<br>sourceProd.<br>cost (\$/kg)Ref.Central steam reformingNatural gas1.5[17,26]Distrib. steam reformingNatural gas2.6[26]GasificationCoal1.2[26]Gasification with CCSCoal1.8[17,26] |
|--|
| Central steam reformingNatural gas1.5[17,26]Distrib. steam reformingNatural gas2.6[26]GasificationCoal1.2[26]Gasification with CCSCoal1.8[17,26]   |
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| Distrib. steam reformingNatural gas2.6[26]GasificationCoal1.2[26]Gasification with CCSCoal1.8[17,26]   |
| GasificationCoal1.2[26]Gasification with CCSCoal1.8[17,26]   |
| Gasification with CCS Coal 1.8 [17,26]   |
|  |
| Distributed electrolysis Grid electricity 6.8 [26]   |
| Central electrolysis Wind 3.8 [26]   |
| Distributed electrolysis Wind 7.3 [26]   |
| Thermochemical cycle Nuclear 1.4 [26]  |
| Pyrolysis/Cracking Natural gas + solar 3.0 [9]   |
| Pyrolysis/Cracking Natural gas + solar 3.6 [10]  |
| Pyrolysis/Cracking Natural gas + solar 4.5 [9]   |
| Steam reforming Natural gas + solar 2.2 [16]   |
| FV electrolysis Solar 9.1 [17]   |
| Solar thermoch. Solar 5.3 [17]   |
| S cycles   |
| Sol. thermoch. Solar 8.3 [17]  |
| oxide/metal  |

Abanades et al., IJHE, 38, 2013.

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• Major drawback for hydrogen due to its extremely low density (problematic for mobility applications)

#### Higher Heating Value per Volume for Different Fuel Options



- Two major storage possibilities:
  - Storage that alters the state or phase:
    - Compression
    - Liquefaction
  - Processes that associate hydrogen to other substances:
    - Adsorption on substrate (e.g. activated carbon)
    - Chemical combination of hydrogen to create hydrogen-rich compound:
      - Hydrogen is tightly bound, requiring chemical process for recovery (e.g. ammonia, methanol)
      - Compounds that can be reversibly transformed into another compound with higher/lower hydrogen content
      - Metal hydrides that can absorb and release hydrogen reversibly when temperature changes

- Compression:
  - Ideal isothermal compression:

$$\frac{W}{m} = p_0 v_0 \ln\left(\frac{p_1}{p_0}\right)$$

Adiabatic compression: •



Ratio of specific heats =  $c_{p}/c_{v}$ = 1.41 for hydrogen at 300 K

- Reality
  - Multi-stage compression with intercooling





- Compression:
  - Quantity of interest gravimetric concentration
  - Described by performance factor:

$$PF = \frac{p_{burst}V}{m_{container}}$$

- Mass of the container is proportional to maximum pressure (just below bursting)
- Only way to improve *PF* is finding better materials
- Currently small quantities are stored in steel pressure cylinders up to 150 bar (e.g. in laboratories), weight 90 kg, *PF* around 250'000 J/kg
- A 500 liter container at 150 bar holds ca. 6 kg of hydrogen which corresponds to 20 liters of gasoline (FC have double efficiency than IC)

- Compression:
  - For very large scale storage: underground formations (aquifers, mines, exhausted natural gas deposit, etc.)
  - Large scale storage in transport pipeline: 1000 km long, 1.2 m diameter at 60 atm → 1000 TJ (~23 mio liters gasoline)

- Liquification:
  - Cooling from 293 to 20 K, and condensation at 20 K and 1 atm, requires theoretically around 14 MJ/kg  $H_{2,1}$
  - But no heat sinks at 20 K exists, multi-stage process needed:

Three-stage propane refrigeration system is used for cooling hydrogen gas from ambient temperature to about 170 K, followed by multistage nitrogen expansion to obtain 77 K, and a multistage helium compression– expansion to complete the liquefaction of hydrogen at 20.3 K and atmospheric pressure

- Liquification:
  - Cooling from 293 to 20 K, and condensation at 20 K and 1 atm, requires theoretically around 14 MJ/kg  $H_{2,1}$
  - Commercial production (Linde Gas AG) reports 54 MJ/kg



- Chemical:
  - Fischer-Tropsch synthesis: use of a catalyst to produce methanol (most widely used catalyst: mixture of Cu, ZnO, and Al<sub>2</sub>O<sub>3</sub>), At 50–100 bar and 250 °C

 $CO + 2 H_2 \rightarrow CH_3OH$ 

• Methanol synthesis:

```
CO_2 + 3 H_2 \rightarrow CH_3OH + H_2O
```

Methanol: can be used in DMFC or ICE, already in liquid form
 Methanol as an energy vector?! But CO<sub>2</sub> has to come from the atmosphere

- Chemical:
  - Metal-hydrides (e.g. CaH<sub>2</sub>, LiH): powdered metals absorb hydrogen under high pressures. With pressure release and applied heat, the process is reversed
  - Have a somewhat bad LCA, and energy intense for production



Comparison

8.6 | gasoline / 100 km = 1 kWh / km 3 | gasoline / 100 km = 0.36 kWh / km



• Comparison

| Storage Media | Volume            | Mass      | Pressure | Temperature |                   |
|---------------|-------------------|-----------|----------|-------------|-------------------|
|               | max. 33 kg H₂·m⁻³ | 13 mass%  | 800 bar  | 298 K       | Composite cylind. |
|               |                   |           |          |             | established       |
|               | 71 kg H₂⋅m⁻³      | 100 mass% | 1 bar    | 21 K        | Liquid hydrogen   |
|               | 20 kg H₂⋅m-³      | 4 mass%   | 70 bar   | 65 K        | Physisorption     |
|               | 150 kg H₂⋅m-₃     | 2 mass%   | 1 bar    | 298 K       | Metalhydrides     |

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# Distribution

• Concept:

Trucks with compressed or liquid hydrogen:



#### Fueling station:





**Transportation services** 

On site generation: By electrolysis and renewable By fossil fuels



- Piped hydrogen
- What about decentralized production, even in the car?

## Distribution

• Hydrogen highway



#### 40 "H2 pumps" on the Highway about 2000 km

## Distribution

- Hydrogen highway
- 3 FC- busses in each city
- Different hydrogen
  Productions





#### **Emerging Renewable Power**

• Outline:

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# Application

- In transportation:
  - Internal combustion:
    - No CO<sub>2</sub> emissions, no smog (sulfur-based, unburned hydrocarbons, CO), no particles, reduction in NO<sub>x</sub>
    - Improved cold starting performance
    - Efficiency similar or slightly higher (higher diffusivity, uniform fuel-air mixtures, minimal ignition energy lower, wide flammability allows to work from lean to stoichiometric mixtures, high ignition temperatures allows to use higher compression ratio)
  - Fuel cells
    - No CO<sub>2</sub> emissions, no smog, no particles, no NO<sub>x</sub>
    - Improved cold starting performance
    - No noise
    - Higher efficiencies (not limited by Carnot)



#### Learning outcomes of todays lecture

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  - How can hydrogen be generated, how renewable
  - How can hydrogen be stored
  - How can hydrogen be transported/distributed
  - Where and how is hydrogen used as an end product

#### **Additional literature**

- Da Rosa: Fundamentals of Renewable Energy Processes, Elsevier, 2005.
- Grimes, Varghese, Ranjan: Light, Water, Hydrogen, Springer, 2008.