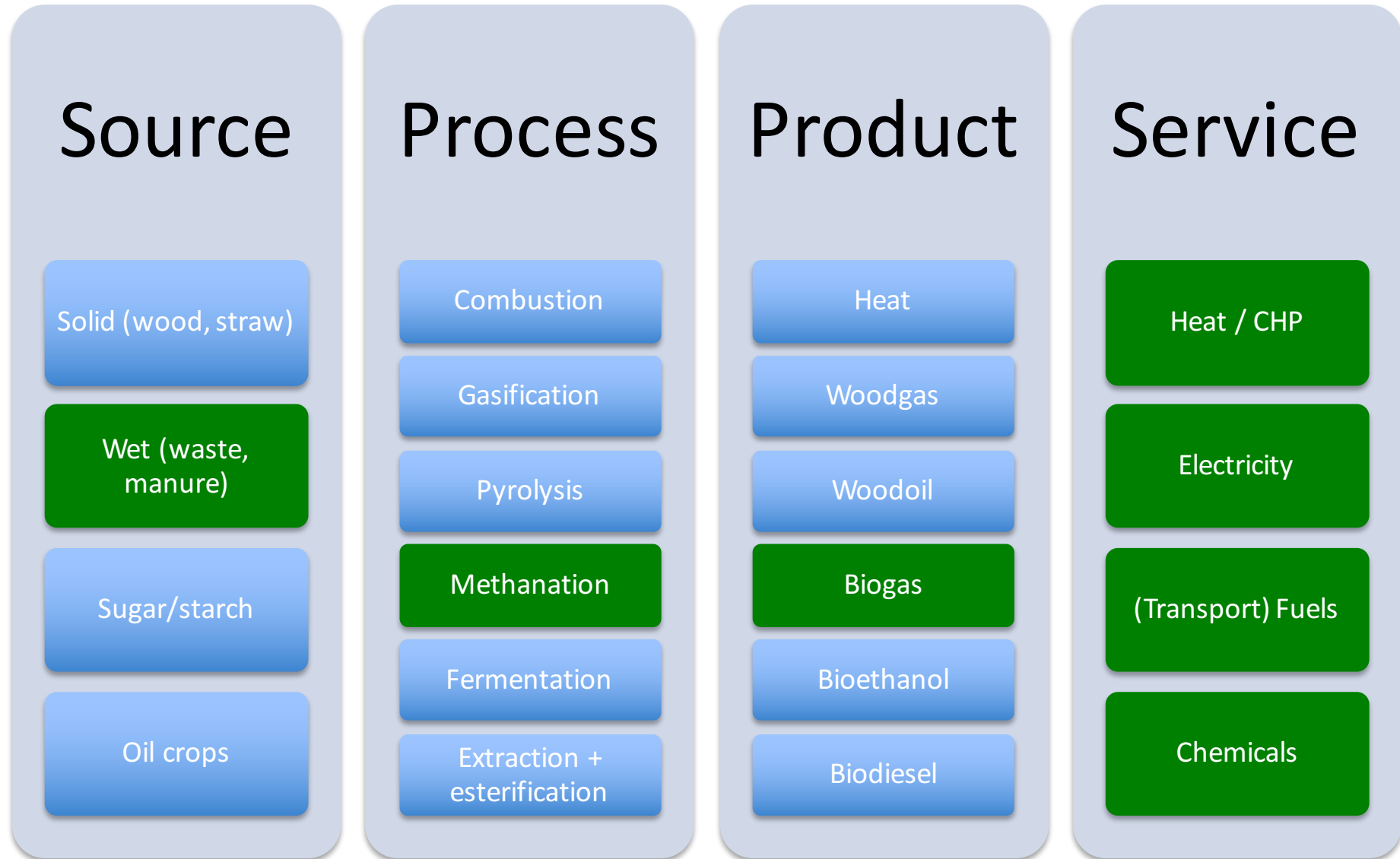


# **Biomass: biogases**

# BIOGAS



# Sources for biogas generation

=> *essentially wet wastes, too inefficient to burn:*

- organic industrial effluents <5% organic dry matter
- sewage 5%
- farming residues 10%
- solid wastes (digesters, landfill) >20%
  - municipalities ( $\approx 20 \text{ m}^3/\text{yr.person}$ ) MSW
  - industry ISW
  - $>100 \text{ m}^3$  biogas produced per tonne 'solid' waste ( $\approx 20\%$  org. solids)  
(ca. 500 L biogas per kg organic dry matter)

# When to *digest* waste?

Waste disposal scheme options, in particular for organics :

- incineration: for **solid** wastes
- composting: = aerobic; for farming (fertilising)
- **methanisation:** = **anaerobic digestion**
- landfill: as a lesser option, when none of the other options apply...; landfilling, however, is restricted in the case of organic wastes

=> most appropriate for **liquid** wastes with an organic fraction

# EU “waste-to-energy hierarchy”

Examples of waste-to-energy processes

Anaerobic digestion of organic waste where the digestate is recycled as a fertiliser

Waste incineration and co-incineration operations with a high level of energy recovery  
Reprocessing of waste into materials that are to be used as solid, liquid or gaseous fuels

Waste incineration and co-incineration operations with limited energy recovery  
Utilisation of captured landfill gas



“The role of waste-to-energy in the circular economy”,  
Brussels, 26.1.2017 COM(2017) 34 final

# Anaerobic digestion - AD (1)

- =transformation of organic matter by microorganisms (bacteria) in **absence of O<sub>2</sub>**
- **internal** reduction + oxidation breakdown of the biomass polymers (C-H-O) to the simplest building blocks :  
**CH<sub>4</sub>** (fully reduced) + **CO<sub>2</sub>** (fully oxidized ) => **biogas**
- mature market technology
- drawback: lignine is nearly undigestable, cellulose is **difficult** to digest  
=> AD is a **slow** process (10-20 days residence time), occurring at  $\approx 35-55^{\circ}\text{C}$

# Digestion process (2)

4 distinct steps in time; using 3 different bacterial groups

## 1. Hydrolysis (uses exo-enzymes)

= the **slowest** of the 4 steps (rate-determining)

breaks solid org. matter down to liquified monomeres & dimeres:

cellulose → cellobiose + glucose

starch → maltose + glucose

## 2. Digestion

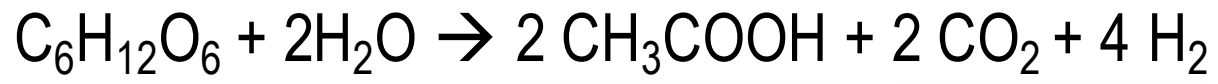
= formation of organic **acids**

acetic / propionic / butyric acid ( $=C_2/C_3/C_4\text{-OOH}$ ), lactic acid, ethanol, and little  $H_2$  and  $CO_2$

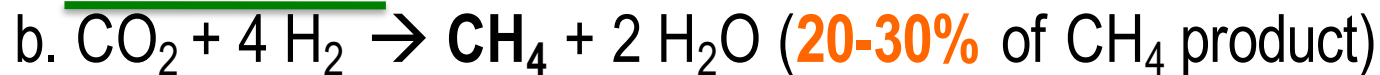
# Digestion process (3)

## 3. 'Acidogenesis'

higher acids break down to  $\text{CH}_3\text{COOH}$  (**acetic acid**),  $\text{H}_2$  and  $\text{CO}_2$ , approximatively as in the overall reaction:

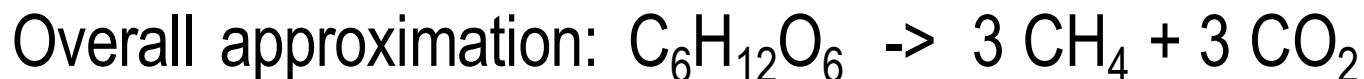


## 4. 'Methanogenesis':



Reactions a & b take place upon different bacterial actions.

These 2 parallel  $\text{CH}_4$ -synthesis reactions explain why biogas compositions typically are  $(60 \pm 5)\%$   $\text{CH}_4$  and  $(40 \pm 5)\%$   $\text{CO}_2$



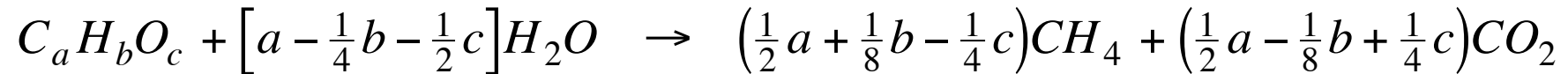


# Anaerobic digestion - AD (4)

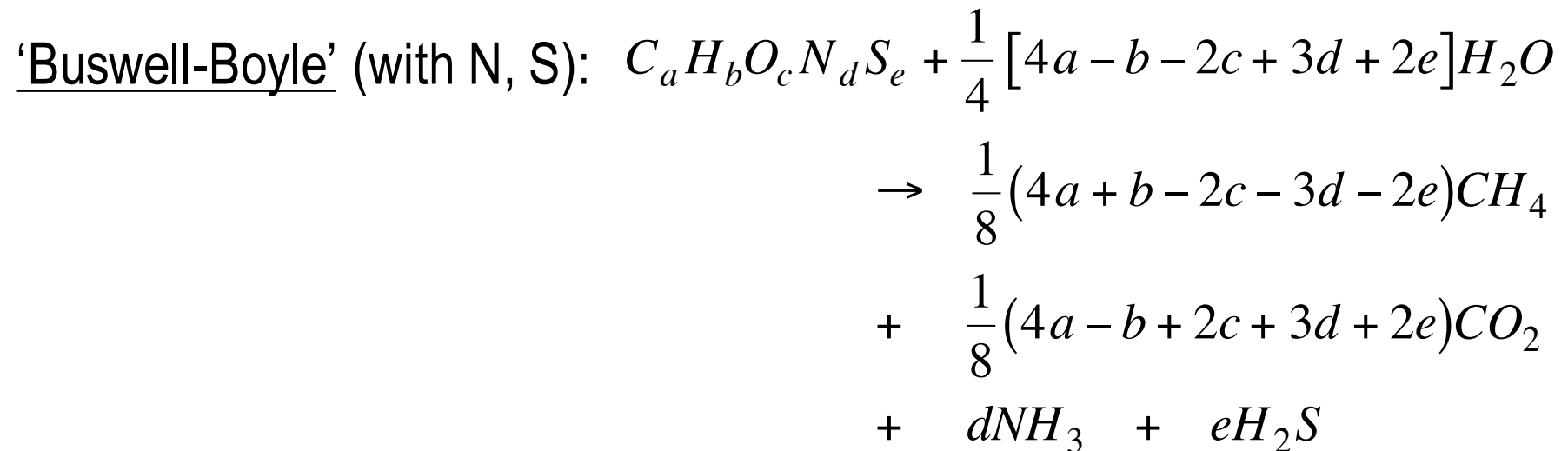
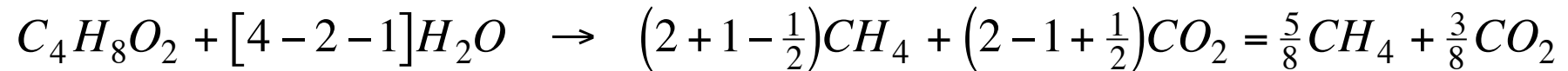
- The main objective for sewage and similar effluents (e.g. food industry) is waste **treatment**, i.e. **depollution** of liquid streams that are too heavily charged in organics, which cannot be discharged directly into the aquatic ecosystem; hence **biogas** is here mainly a **by-product** (energy recovered to power the “depollution plant”)
- However, in the case of largely untapped farm waste (manure, crop residues) and MSW/ISW, biogas is not a by-product but an active **energy vector** (and especially for valorisation into **electricity** production, in gas **engines** or **fuel cells**)

# Chemical formulae for biogas generation

'Buswell' formula:



e.g. for **manure**, approximated as  $C_4 H_8 O_2$  (butyric acid):



Remark:  $CO_2$ ,  $NH_3$ ,  $H_2S$  dissolve better in  $H_2O$  than  $CH_4$ ,  
hence the recovered gas is actually methane-enriched

# Digestion is a batch process

- once a day, fresh organic substrate is filled in, and digested matter is removed from a batch reactor

- mean residence time (days):

– saturation after 20 days

$$\theta = \frac{V_{reactor} [m^3]}{\dot{V}_{org} [m^3/d]}$$

- daily specific load (kg/m<sup>3</sup>.d)

– M can designate fresh or dry organic matter

$$M_{day} = \dot{V}_{org} \cdot \frac{M}{V} = \frac{M}{\theta}$$

- biogas production can be expressed as:

$$\frac{m^3_{biogas}}{m^3_{reactor}}$$

$$\frac{m^3_{biogas}}{kg_{org.matter}}$$

# Example:

Farm with 60 animals. Manure waste: 3 m<sup>3</sup>/day. (≈3000 kg)

Organic dry matter = 50 kg/m<sup>3</sup> (=150 kg/day=5% organics)

Mean residence time  $\theta$  = 20 days. Biogas production = 65 m<sup>3</sup>/day. (≈433 L / kg d.m.)

- Reactor volume :  $V_{reactor} [m^3] = \theta \cdot \dot{V}_{org} = 20 * 3 = 60m^3$

- Daily specific load:  $M_{day} = \frac{M_{org}}{\theta} = \frac{50kg/m^3}{20days} = 2.5kg/m^3 \cdot day$

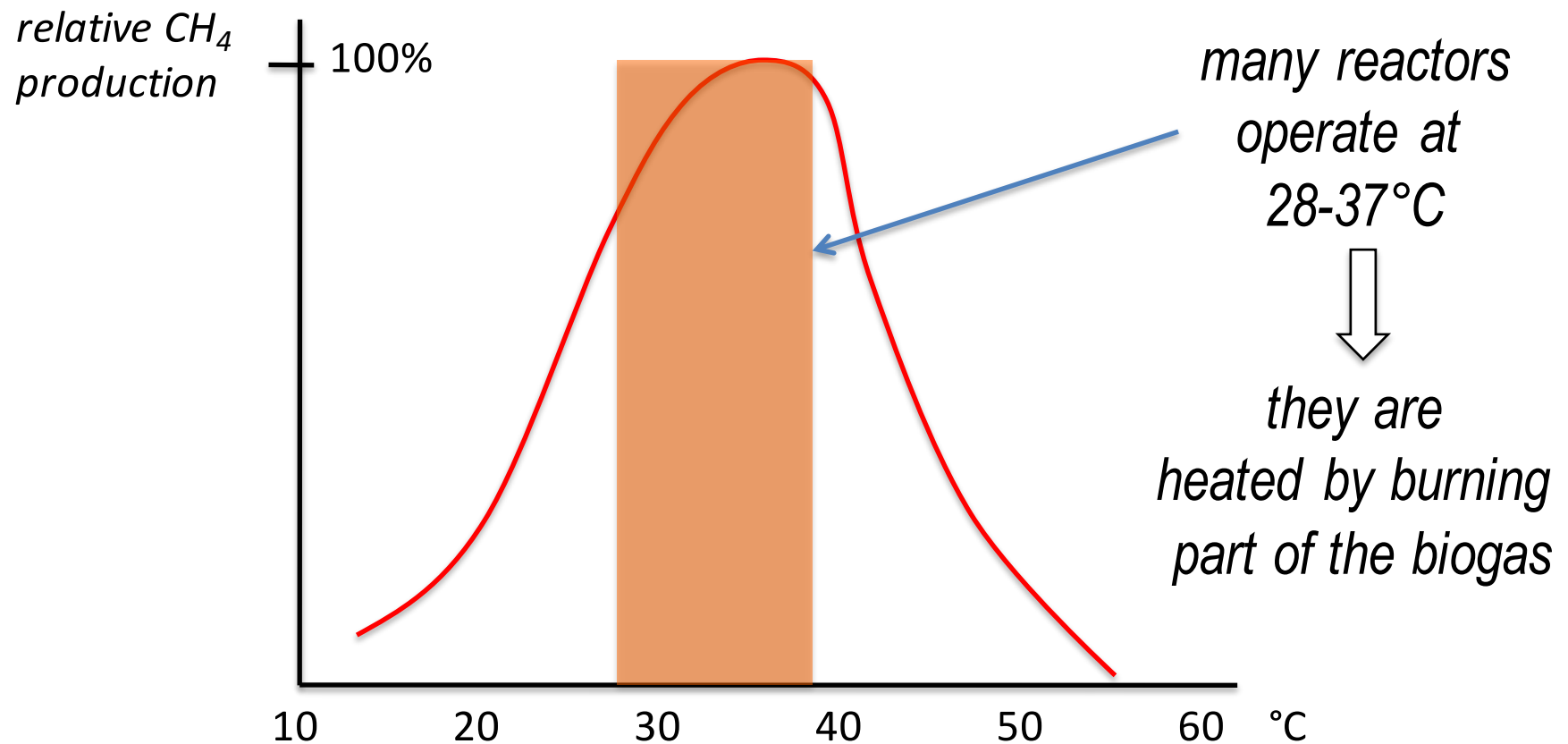
- Specific biogas production:
  - per reactor volume:  $P = \frac{65m^3/d}{60m^3} = 1.08 \frac{m^3/d}{m^3}$

- per organic matter:

$$P = \frac{65m^3/day}{M_{org} \left[ \frac{kg}{m^3} \right] \cdot V_{reactor} [m^3] / \theta [days]} = \frac{65}{50 \cdot \frac{60}{20}} = 0.43 \frac{m^3}{kg_{org.matter}}$$

# Digester reactor temperature

Enzyme	Optimal T range
'Psychrophilic'	20°C
'Mesophilic'	20-45°C
'Thermophilic'	>45°C



# Experience values

- The determining factors in biogas production are:
  - **temperature**; part of the biogas is used to heat the reactor; the biogas production rate saturates at 40°C
  - **residence time** (days); saturates at 20 days
  - **organic matter charge** (usually 3-10%)

Production	Unit	Cows	Pigs
per animal and day	$m^3_{biogas} / head.day$	1.3 ± 0.3	1.5 ± 0.6
per mass	$m^3_{biogas} / kg_{org.matter}$	0.3 ± 0.05	0.5 ± 0.05

→ 1.5 m<sup>3</sup>/day @ 20 MJ/m<sup>3</sup> = 30 MJ/day ≈ 8 kWh/day

= equivalent to 2 m<sup>2</sup> of thermal solar collectors

Any farm animal produces ca. 18-20 kg of manure per year per kg of its own body weight

# Biogas vs. natural gas

Property	Unit	NG	BG (60% CH <sub>4</sub> )
LHV	MJ / m <sup>3</sup>	36	21.5
Density	kg/m <sup>3</sup>	0.82	1.21
Ignition T	°C	620	700
Ignition speed in air	m/s	39	0.25
Air factor	-	9.5	5.7
Exhaust, max CO <sub>2</sub>	Vol%	11.9	17.8
Exhaust, dew point	°C	59	60-160

# Some characteristics of biogas production

- the digestate is a good quality **fertilizer** (2% nitrogen)
  - better than (air-)composted waste (<1% nitrogen)
- a significant part of the produced biogas is used for **heating of the digester** and the installation itself (farm,...)
- (cold) **desulfurisation** of the biogas is done with  $\text{FeCl}_3$  solution (to precipitate  $\text{FeS}$ ); sulfur is removed as it is poisonous (for the atmosphere but also in downstream CHP engines or fuel cells)



# Biogas use and potential (EU)

Source	2007 Use (PJ)	gas engines ↑ kW <sub>e</sub> /site	ultimate Potential
Effluents	7	200 kW	140 PJ
Sewage	37	50-200	215
Manure	30	10-100	750
Solid agro	45		1370
MSW,ISW	15	0.1-1 MW	330
Landfill	120	1 MW	-
<b>TOTAL</b>	<b>254 PJ</b> (6 Mtoe)	<i>huge margin</i> →	<b>2805 PJ</b> (67 Mtoe)

↓ 30% efficiency  
**20 TWh<sub>el</sub>**  
**(0.6% of total)**

↓  
 =25% of NG import in EU

# Biogas application examples (CH)

Source	Biogas m <sup>3</sup> /day	% CH <sub>4</sub>	% yr load	Installed power	Effi- ciency
Farm 37 cattle	70	57	60	<b>5 kW<sub>el</sub></b>	<b>18%</b>
Sewage 30'000 p.	1000	65	65	<b>130 kW<sub>el</sub></b>	<b>28%</b>
MSW 80'000 p.	1300	60	95	<b>90 kW<sub>el</sub></b>	<b>25%</b>

*=> small power sites (gas engines); low (electrical) efficiency*

# Special case of landfill gas (LFG)

- (multi)MW<sub>el</sub>-size sites (with gas engines, gas turbines)
- an important fraction of world biogas (20 Mtoe)
- 3 Mtoe in EU-27
- important anthropogenic **GHG emitter!** (as CH<sub>4</sub>)
- often heavily contaminated (with F, Cl, NH<sub>3</sub>, H<sub>2</sub>S, Si,...)
- often of low calorific value (diluted with N<sub>2</sub>/O<sub>2</sub>)
  - engines stop running <45% CH<sub>4</sub>
  - **fuel-assisted flaring or venting !**