

# Assignment #1 Aquasim for BOD<sub>5</sub> measurement

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Note: This is your first assignment which is quite consequent.

The prerequisite is to have fulfilled the basic **(Self-)Training of Aquasim!**

**Don't remain alone and stuck** if you don't catch or understand the problem... **Use intensively the Moodle forum** (all together and with teacher assistants)!

**SHARE TOGETHER and again, write up personally!**

For your convenience, **please follow the assignment step by step!**

→ Provide .DOC and .PDF file with your answer with plots and the Aquasim files .AQU (including calculations) you used to solve this assignment (1 .DOC + 1 .PDF +2 .AQU files)

## A1. INTRODUCTION - BOD<sub>5</sub> Measurement (design)

The BOD<sub>5</sub> is a biological estimation of the organic content (pollution) in a wastewater sample.

Definition from:

[http://en.wikipedia.org/wiki/Biochemical\\_oxygen\\_demand](http://en.wikipedia.org/wiki/Biochemical_oxygen_demand)

Biochemical oxygen demand or BOD is a chemical procedure for determining the amount of dissolved oxygen needed by aerobic biological organisms in a body of water to break down organic material present in a given water sample at certain temperature over a specific time period. It is not a precise quantitative test, although it is widely used as an indication of the organic quality of water.[1] . It is most commonly expressed in milligrams of oxygen consumed per liter of sample during 5 days of incubation at 20 C and is often used as a robust surrogate of the degree of organic pollution of water.

See also Lecture on COD Balance



By definition, the BOD<sub>5</sub> is given by the O<sub>2</sub> depletion due to the O<sub>2</sub> uptake rate after 5 days of organic pollution biodegradation in a wastewater sample.

In other words, it's the amount of O<sub>2</sub> consumed at 20°C in a S.T.R. - Stirred Tank Reactor in batch mode, during 5 days with known initial conditions:

- dissolved O<sub>2</sub> concentration (**S\_O2ini**) is set with the dilution fresh water saturated in O<sub>2</sub> with air
- initial organic content (diluted sample) (**S\_Sini**)
- initial biomass (diluted activated sludge) (**X\_Hini**)

For these DBO<sub>5</sub> tests are provided:

1. An 0.5 Liter bottle with a magnetic stirrer in a temperature controlled room 20°C.
2. A domestic wastewater sample with a supposed BOD<sub>5</sub> of 300 mg O<sub>2</sub>/L (400mg COD/L)
3. An inoculum of fresh activated sludge at 3.5 g TSS/L (1.36\*3.5\*1000=4760mgCOD/L)

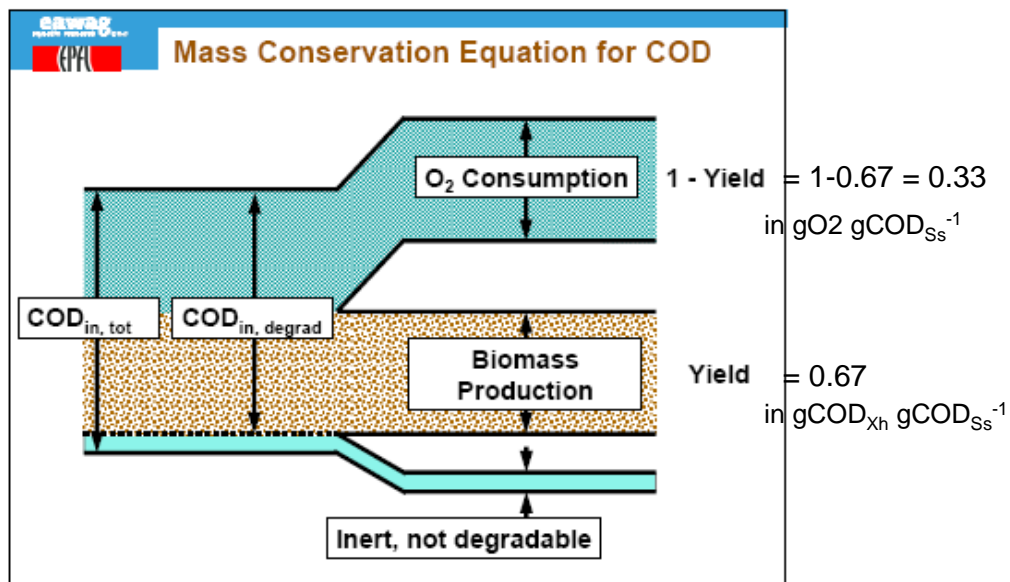
From Lectures about BOD, one can consider the COD balance of a perfectly biodegradable organic matter:

$$- \text{COD}_S + \text{BOD} + Y_{\text{COD}} * \text{COD}_S = 0$$

(Here  $Y_{\text{COD}} = Y_H$  (see p 24 of ASM1\_FinalVersion.pdf in provided Readings))

Thus the  $\text{BOD}_5$  is just a fraction of the COD of the sample which corresponds to the  $\text{O}_2$  consumption required for biodegradation of a given consumed COD. The rest is assimilated/incorporated by the biomass growth. The  $\text{BOD}_5$  measurement is fundamentally a respiration of the biomass and a fraction of the COD consumed depending of  $Y_{\text{COD}}$  biomass over substrate yield (which depends strongly on the organic matter).

## COD balance



From Siegrist H., SIWWTP-09

Ideally, to be a good organic matter measurement of a wastewater sample, a  $\text{BOD}_5$  measurement test in a biodegradation agitated flask (batch mode) should respect:

- 1) **No limitation of available  $\text{O}_2$ .** At the end of this batch, the  $\text{O}_2$  dissolved oxygen concentration shouldn't be below 10 or 20 % of the  $\text{O}_2$  saturation. To improve your modeling to avoid an underestimation of the  $\text{BOD}_5$  due to oxygen limitation, you can complete the growth process (built during your Aquasim self-training) with an  $\text{O}_2$  Switching Function (see p 11 ASM1\_FinalVersion.pdf and consider Heterotrophic growth process #1 with  $K_{\text{O,H}}$  constant p 24).
- 2) **Full substrate consumption.** As much as possible of the initial substrate loaded into the  $\text{DBO}_5$  test bottle, should be consumed by respirometry during these 5 days

Overestimation of the  $\text{BOD}_5$  can be due to:

- a. The biodegradation/consumption (*Death regeneration*) of the decayed biomass (with implies a second growth (and respiration) of the COD already “anabolised” one time in biomass)
- b. or *Endogenic respiration* of the already grown biomass (which is a bias of the estimation of the organic matter measured by BOD<sub>5</sub> test. The respiration of grown biomass on sample organic matter is not respiration of growth on initial organic matter of the sample)

There requirements of good DBO<sub>5</sub> measurement should be fulfilled and these bias should be minimized!

Your duty is using Aquasim batch dynamic simulation to **design the BEST measurement experiment by choosing:**

- The **right INITIAL dilution (i.e. the initial organic load) of the wastewater sample to be measured**
- The **right INITIAL inoculum** (activated sludge) concentration

For this duty, please follow the procedure bellow:

A1.I. **COD Balance preliminary approach**

In first approximation you can use a COD mass balance approximation of the bioprocess occurring in the BOD<sub>5</sub> test flask. This will allow a first estimation of initial substrate organic load that could be poured in the test bottle, which allows the consumption of 90% of the maximum dissolved O<sub>2</sub> (saturation).

A1.II. **Aquasim simulation approach BOD<sub>5</sub> modeling on the basis on ASM1 Heterotrophic growth and decay**

Then using dynamic simulations of the simplified ASM1 modeling in Aquasim (intro\_batch.AQU) you would find the best initial values (i.e. experimental conditions) of the BOD<sub>5</sub> tests, which will satisfy the above requirements.

This allow you to find by (trials and errors) the 3 states variables S<sub>S</sub>, X<sub>H</sub>, S<sub>O</sub> initial values for the best measurement of the BOD<sub>5</sub> of the given wastewater sample.

B.1. **BOD<sub>5</sub> Test Preparation**

Lastly, from these values you will provide the diluted concentration of each sample, O<sub>2</sub> saturated water and biomass inoculum to fill in the 0.5L BOD<sub>5</sub> flask.

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**A1.I. COD Balance preliminary approach (2)**

Comes back to “Microbial Stoichiometry (undefined systems)” lecture and consider COD mass balance equation:

$$- \text{COD}_S + \text{BOD} + Y_{\text{COD}} * \text{COD}_S = 0$$

$$\rightarrow Y_{\text{COD}} = 1 - (\text{BOD} / \text{COD}_S)$$

$$\rightarrow Y_{\text{H,X}} = \text{grown X/consumed S} = (Y_{\text{COD}} * \text{COD}_S) / \text{COD}_S = Y_{\text{COD}}$$

On a first approach, on the basis of the COD balance, and knowing the Y<sub>COD</sub> = Y<sub>H</sub> yield (see p 24 of ASM1\_FinalVersion.pdf in “Moodle” Readings provided).

From this COD mass balance, one can:

- 1) Rewrite (equilibrate) COD mass balance equation with the  $Y_{\text{COD}} = Y_{\text{H}}$  yield.
- 2) Rewrite the obtained COD mass balance equation by fixing the maximum BOD (90% of dissolved O<sub>2</sub> saturation) which can be consumed during the 5 days respiration. (As BOD is known at 90% of O<sub>2</sub> saturation, 1<sup>st</sup> estimation of COD<sub>S</sub> is available. It is a first estimation of  $S_{\text{Sini}}$  ...)

Based on this theoretical COD mass balance calculation, give the amount of biomass produced, substrate consumed and the amount of O<sub>2</sub> consumed. These 3 values are estimations of what could be the initial values for dynamic simulation:

- COD<sub>S</sub> →  $S_{\text{Sini}}$
- BOD → O<sub>2</sub> requirement which should be less than 90% of the maximum Dissolved O<sub>2</sub> saturation (9.1mgO<sub>2</sub>/L) →  $S_{\text{O2ini}}$
- $Y_{\text{COD}} \times \text{COD}_S \rightarrow \text{Final } X_{\text{H}}$

### A1.II. Aquasim simulation approach BOD<sub>5</sub> modeling on the basis on ASM1 Heterotrophic growth and decay (5)

This COD balance approach is somewhat not satisfying as it doesn't take into account the biomass decay/endogenic respiration/biomass OR death regeneration phenomenon occurring in the BOD<sub>5</sub> bottle. This phenomenon is rather significant in the BOD<sub>5</sub> test, as measurement lasts for 5 days in batch mode with a quite low the specific growth rate. Use of Aquasim and ASM1 modeling can cope with these phenomena!

You may consider the 2 simplest models you had built during Aquasim Self-Training which differ only on the stoichiometry of the decay process

In both case, use kinetic model parameters and yield coefficients (20°C) from AMS1 IWA Model for  $Y_{\text{H}}$ ,  $K_{\text{S}}$ ,  $K_{\text{O,H}}$ ,  $\mu^{\text{max}}_{\text{H}}$ ,  $b_{\text{H}}$  (see **ASM1\_FinalVersion.pdf ASM1 document (p24)**)

You will have to complete/modify these simplest ASM models (Endogenic respiration AND Death Regeneration)) with a switching function for O<sub>2</sub> for the growth process (see **ASM1\_FinalVersion.pdf ASM1 document (p11) process#1**) to take into account this O<sub>2</sub> limitation.

Endogenic respiration (presented in the Training MD Aquasim ASM-TUUH and in ASM1_FinalVersion.pdf)						Death regeneration							
Component	→	i	1	2	3	Process Rate, $\rho_j$	Component	→	i	1	2	3	Process Rate, $\rho_j$
j	Process	↓	$X_{\text{B}}$	$S_{\text{S}}$	$S_{\text{O}}$	$[\text{ML}^{-3} \text{T}^{-1}]$	j	Process	↓	$X_{\text{B}}$	$S_{\text{S}}$	$S_{\text{O}}$	$[\text{ML}^{-3} \text{T}^{-1}]$
1	Growth		1	$-\frac{1}{Y}$	$-\frac{1-Y}{Y}$	$\frac{\mu S_{\text{S}}}{K_{\text{S}} + S_{\text{S}}} X_{\text{B}}$	1	Growth		1	$-\frac{1}{Y}$	$-\frac{1-Y}{Y}$	$\frac{\mu S_{\text{S}}}{K_{\text{S}} + S_{\text{S}}} X_{\text{B}}$
2	Decay		-1		-1	$b X_{\text{B}}$	2	Decay		-1	1		$b X_{\text{B}}$
Observed Conversion Rates $\text{ML}^{-3} \text{T}^{-1}$						Kinetic Parameters: Maximum specific growth rate: $\mu$ Half-velocity constant: $K_{\text{S}}$ Specific decay rate: $b$	Observed Conversion Rates $\text{ML}^{-3} \text{T}^{-1}$			$r_i = \sum_j r_{ij} = \sum_j v_{ij} \rho_j$			Kinetic Parameters: Maximum specific growth rate: $\mu$ Half-velocity constant: $K_{\text{S}}$ Specific decay rate: $b$
Stoichiometric Parameters: True growth yield: $Y$			Biomass $[\text{M}(\text{COD}) \text{L}^{-3}]$	Substrate $[\text{M}(\text{COD}) \text{L}^{-3}]$	Oxygen (negative COD) $[\text{M}(-\text{COD}) \text{L}^{-3}]$		Stoichiometric Parameters: True growth yield: $Y$			Biomass $[\text{M}(\text{COD}) \text{L}^{-3}]$	Substrate $[\text{M}(\text{COD}) \text{L}^{-3}]$	Oxygen (negative COD) $[\text{M}(-\text{COD}) \text{L}^{-3}]$	

As in this Aquasim model file **intro\_batch.aqu** you had implemented an oxygen transfer process called “oxygen\_trans”, which is not valid for the present purpose. The BOD<sub>5</sub> estimation is a respirometry measurement and where there is NO O<sub>2</sub> transfer, as it occurs in a sealed bottle. Indeed, for this BOD<sub>5</sub> measurement, the amount of O<sub>2</sub> is fixed/provided initially and the bioprocesses occurs in a batch mode in a closed 0.5 L bottle without any O<sub>2</sub> transfer. You could cancel this Aquasim process by many manners:

- Inactivate the O<sub>2</sub> transfer process in the process windows of *the compartment (batch reactor) component windows*
- Delete the process in the *process windows*
- Set the k<sub>LA</sub> oxygen transfer time constant or set S\_O2\_Sat constant to Zero

According the 2 approaches (**Endogenic respiration** and **Death regeneration**) you will provide 2 Aquasim simulation files .AQU.

### **A1.II.a. Mass balance equations and model parameters (3)**

To be sure of your understanding provide and write down:

1. The **mass balance equations** for your 3 state variables X<sub>H</sub> (X\_H), S<sub>S</sub> (S\_S), S<sub>O2</sub> (S\_O), for the **2 modeling approaches** (i.e. the 3 differential equations for each model – See bioprocesses of ASM1 PDF p 11)
2. A **table of model parameters and kinetic parameters** you will used in yours simulations (See ASM1 PDF Table 5 p 24)

### **A1.II.b. BOD<sub>5</sub> Simulations (4)**

Once, your two (endogenic/death-regeneration) BOD<sub>5</sub> ASM model are ready, on the basis of the COD balance equation, you can compute the theoretical BOD in the effluent (g COD of substrate) according the balance and the Y<sub>COD</sub>, biomass yield on substrate.

Use as “starting point” the Aquasim model you create during Training MD Aquasim ASM-TUUH, i.e. the Aquasim file **intro\_batch.aqu**. You can modify it, according what is explained A1.II.a (above)

From the previous COD mass balance approach A1.I, considering this COD global growth equation in 1L volume, you had obtained a first estimation of the S<sub>S,ini</sub> concentration (COD<sub>S</sub> substrate to be consumed) and the X<sub>H,Fin</sub> concentration (Y<sub>COD</sub> x COD<sub>S</sub> biomass produced). Thus for your 1st Aquasim simulation, you can use these values as initial values:

- S<sub>S,ini</sub> for S<sub>S</sub>
- S<sub>O2,ini</sub> = S<sub>O2sat</sub> = 9.1 mg/L
- X<sub>H,ini</sub> = X<sub>H,Fin</sub> /100

Probably, your first simulated results will dissatisfy the criteria we mention above... Why?

The COD balance equation is a “theoretical” biomass growth equation rather than a real “observable”. The COD balance, in the Matrix formulation modelling is dependent on the “Endogenic respiration” or “Death regeneration” which have been taken into account in your models.

Note: About the strange behavior of modeling **DBO5 –Endogenic Respiration** (increase of S<sub>S</sub> when S<sub>O2</sub> drops to 0! This is an artifact of the Growth rate process calculation in which S<sub>O2</sub> which a state variable which can't be negative by definition, but which is decreased bellow 0 due to the Decay rate having the stoichiometric coefficient = -1 (this decay process is going on even if S<sub>O2</sub> <=0. To solve the behavior an IF test on S<sub>O2</sub><=0 could be set in the Growth process formula!) (To check the artifact, one can build for plotting, two Formula Variables, Decay and Growth with the same formulas as the two modeled processes). This artifact isn't

observed in the modeling **DBO5\_Lyse** (Death/Regeneration) in which lysed biomass becomes new substrate  $S_S$ . In fact the dynamic of the 1<sup>st</sup> modeling is only valid when  $S_{O2}$  stay above zero along the simulation!

**By changing  $S_{S,ini}$  and  $X_{H,ini}$  with trials and errors, try to find YOUR best BOD<sub>5</sub> initial conditions.**

To help you, to find the initial simulation conditions that will allow the best BOD<sub>5</sub> measurement, a non-subjective criterion is to calculate, for each simulation, the observed  $Y_{COD}$  yield at the end of the simulation (i.e. the BOD<sub>5</sub> measurement). Remembering:

$$-COD_S + BOD + Y_{COD} * COD_S = 0$$

$$\rightarrow Y_{COD} = 1 - (BOD / COD_S)$$

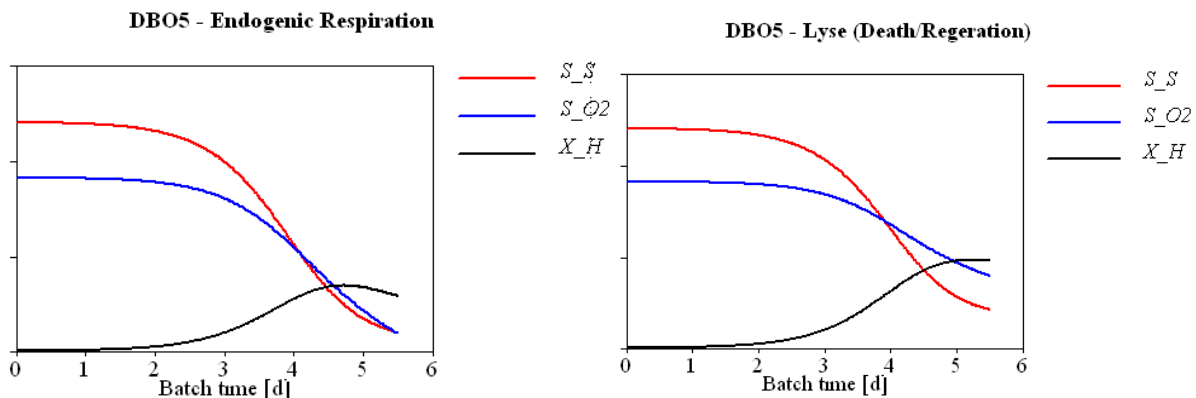
Thus, from simulation:

- $COD_S \approx \Delta S_S$
- $BOD \approx \Delta S_{O2}$
- $Y_{COD,obs} = 1 - (\Delta S_{O2} / \Delta S_S)$

This  $Y_{COD,obs}$  estimation should be as closest as possible to the theoretical  $Y_{COD}$  of COD mass balance equation, see A1.I.).

In others words, try to find the best simulation conditions, which compute the least “biased” (due to Endogenic respiration or Death/Regeneration) simulation of the BOD<sub>5</sub> measurement, trying to be closest to the Theoretical COD mass balance.

By trials and errors you may find YOUR good compromise dynamic behaviors which can look like the figures below:



Auto Checking: To check the effect of “Endogenic respiration” or “Lyse – Death/Regeneration” you can invalidate them in your 2 modellings, and check that you will retrieve a theoretical COD mass balance growth... ;-)))

### **B.1 BOD<sub>5</sub> Test Preparation (3)**

Using your best initial simulated values ( $S_{S,ini}$ ,  $S_{O2,ini}$ ,  $X_{H,ini}$ ) setup your experiment in the 0.5L bottle to measure the BOD<sub>5</sub>. Calculate the dilution required from the wastewater sample and the required activated sludge inoculum, that respect your choice to do the best BOD<sub>5</sub> measurement (i.e. (i) wastewater sample volume, (ii) activated sludge biomass inoculum volume and (iii) saturated O<sub>2</sub> fresh water for dilution).

Note: Dilution formula mass conservation with dilution

$$C1.V1 = C2.V2 \quad [mgCOD.L^{-1}. L = mg COD]$$

May be a comment of these calculations?

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Note: In fact in Standard Methods DBO<sub>5</sub> measurement protocol, the amount of S<sub>S</sub> (organic pollution to be measured) and S<sub>O2</sub>, are not fixed as here. The standard protocol, fixe the S<sub>S</sub> and S<sub>O2</sub> proportion by the ration of two volumes, the sample non diluted volume, which implies a gas phase volume complement to the 0.5L of the bottle. This allows two benefits: 1) as there is much more O<sub>2</sub> in air (21%) than in air saturated water, the amount of COD<sub>S</sub> to be measured could be more important 2) the measurable gas phase depletion would be greater for more accuracy. This could be modeled using gas transfer phenomenon, but it couldn't be proposed here, as you will learn it, later in the course.