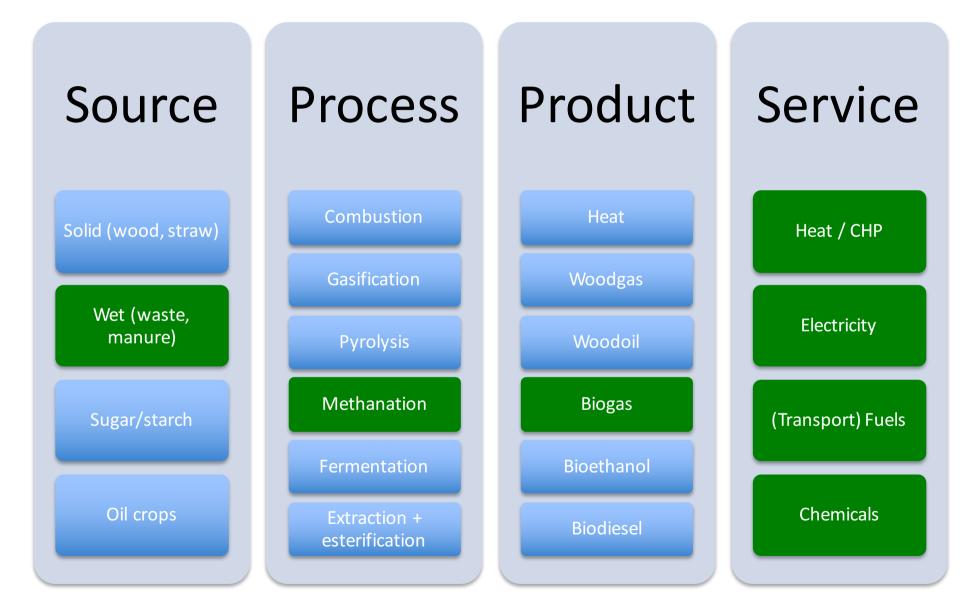
# Biomass: biogases

#### BIOGAS



## Sources for biogas generation

#### => essentially wet wastes, too inefficient too burn:

<ul> <li>organic industrial effluents</li> </ul>	<5% organic dry matter
<ul> <li>sewage</li> </ul>	5%
<ul> <li>farming residues</li> </ul>	10%
<ul> <li>solid wastes (digesters, landfill)</li> </ul>	>20%
<ul> <li>municipalities (≈20 m<sup>3</sup>/yr.person)</li> </ul>	MSW
<ul> <li>industry</li> </ul>	ISW
- >100 m <sup>3</sup> biogas produced per tonne	'solid' waste (≈20% org. solids)

 - >100 m<sup>3</sup> biogas produced per tonne 'solid' waste (≈20% org. solids) (ca. 500 L biogas per kg organic dry matter)

#### When to digest waste?

Waste disposal scheme options, in particular for organics :

- incineration:
- composting:
- methanisation:
- landfill:

for **solid** wastes

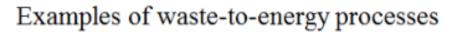
= aerobic; for farming (fertilising)

#### = anaerobic digestion

as a lesser option, when none of the other options apply...; landfilling, however, is restricted in the case of <u>organic</u> wastes

#### => most appropriate for liquid wastes with an organic fraction

### EU "waste-to-energy hierarchy"



Anaerobic digestion of organic waste where the digestate is recycled as a fertliser

Waste incineration and co-incineration operations with a high level of energy recovery Reprocessing of waste into materials that are to be used as solid, liquid or gaseous fuels

Waste incineration and co-incineration operations with limited energy recovery Utilisation of captured landfill gas

**"The role of waste-to-energy in the <u>circular economy</u>", Brussels, 26.1.2017 COM(2017) 34 final** 



## **Anaerobic** digestion - AD (1)

- =transformation of organic matter by microorganisms (bacteria) in absence of O<sub>2</sub>
- internal reduction + oxidation breakdown of the biomass polymers (C-H-O) to the simplest building blocks :

**CH**<sub>4</sub> (fully reduced) + **CO**<sub>2</sub> (fully oxidized) => biogas

- mature market technology
- drawback: lignine is nearly undigestable, cellulose is difficult to digest

=> AD is a slow process (10-20 days residence time), occurring at ≈35-55°C

## **Digestion** process (2)

4 distinct steps in time; using 3 different bacterial groups

#### 1. Hydrolysis (uses exo-enzymes)

= the *slowest* of the 4 steps (<u>rate-determining</u>)

breaks solid org. matter down to liquified monomeres & dimeres:

cellulose  $\rightarrow$  cellobiose + glucose

starch  $\rightarrow$  maltose + glucose

#### 2. Digestion

= formation of organic acids

acetic / propionic / butyric acid (= $C_2/C_3/C_4$ -OOH), lactic acid, ethanol, and little H<sub>2</sub> and CO<sub>2</sub>

## **Digestion** process (3)

#### 3. 'Acidogenesis'

higher acids break down to  $CH_3COOH$  (acetic acid),  $H_2$  and  $CO_2$ , approximatively as in the overall reaction:

 $C_6H_{12}O_6 + 2H_2O \rightarrow 2 CH_3COOH + 2 CO_2 + 4 H_2$ 

4. 'Methanogenesis': a.  $2CH_3COOH \rightarrow 2 CH_4 + 2 CO_2$  (70-80% of  $CH_4$  product)

b.  $CO_2 + 4 H_2 \rightarrow CH_4 + 2 H_2O$  (20-30% of  $CH_4$  product)

Reactions a & b take place upon different bacterial actions. These 2 parallel  $CH_4$ -synthesis reactions explain why biogas compositions typically are (60±5)%  $CH_4$  and (40±5%)  $CO_2$ 

Overall approximation:  $C_6H_{12}O_6 \rightarrow 3CH_4 + 3CO_2$ 

### **Anaerobic** digestion - AD (4)

- The main objective for <u>sewage and similar effluents</u> (e.g. food industry) is waste treatment, i.e. depollution of liquid streams that are too heavily charged in organics, which cannot be discharged directly into the aquatic ecosystem; hence biogas is here mainly a by-product (energy recovered to power the "depollution plant")
- However, in the case of largely untapped <u>farm waste</u> (manure, crop residues) and <u>MSW/ISW</u>, biogas is not a byproduct but an active <u>energy vector</u> (and especially for valorisation into electricity production, in gas <u>engines</u> or <u>fuel cells</u>)

### Chemical formulae for biogas generation

#### <u>'Buswell' formula:</u>

 $C_a H_b O_c + \left[a - \frac{1}{4}b - \frac{1}{2}c\right] H_2 O \rightarrow \left(\frac{1}{2}a + \frac{1}{8}b - \frac{1}{4}c\right) C H_4 + \left(\frac{1}{2}a - \frac{1}{8}b + \frac{1}{4}c\right) C O_2$ e.g. for **manure**, approximated as  $C_4H_8O_2$  (butyric acid):  $C_4 H_8 O_2 + [4 - 2 - 1] H_2 O \rightarrow (2 + 1 - \frac{1}{2}) C H_4 + (2 - 1 + \frac{1}{2}) C O_2 = \frac{5}{8} C H_4 + \frac{3}{8} C O_2$ <u>'Buswell-Boyle'</u> (with N, S):  $C_a H_b O_c N_d S_e + \frac{1}{4} [4a - b - 2c + 3d + 2e] H_2 O_c$  $\rightarrow \frac{1}{8}(4a+b-2c-3d-2e)CH_4$ +  $\frac{1}{8}(4a - b + 2c + 3d + 2e)CO_2$ +  $dNH_3$  +  $eH_2S$ 

<u>Remark</u>:  $CO_2$ ,  $NH_3$ ,  $H_2S$  dissolve better in  $H_2O$  than  $CH_4$ , hence the recovered gas is actually methane-enriched

## **Digestion is a batch process**

- once a day, fresh organic substrate is filled in, and digested matter is removed from a batch reactor
- mean residence time (days):
  - saturation after 20 days

$$\theta = \frac{V_{reactor} \left[ m^3 \right]}{V_{org} \left[ m^3 / d \right]}$$

- daily specific load (kg/m<sup>3</sup>.d)
- $M_{day} = V_{org} \cdot \frac{M}{V} = \frac{M}{\theta}$ - M can designate fresh or dry organic matter
- biogas production can be expressed as:

 $m^3$ biogas m<sup>3</sup>reactor m<sup>3</sup>biogas/

#### **Example:**

Farm with 60 animals. Manure waste:  $3 \text{ m}^3/\text{day}$ . ( $\approx 3000 \text{ kg}$ ) Organic dry matter =  $50 \text{ kg/m}^3$  (=150 kg/day=5% organics) Mean residence time  $\theta$  = 20 days. Biogas production =  $65 \text{ m}^3/\text{day}$ . ( $\approx 433 \text{ L}$  / kg d.m.)

• Reactor volume :

$$V_{reactor}\left[m^3\right] = \theta . V_{org} = 20 * 3 = 60m^3$$

• Daily specific load:

$$M_{day} = \frac{M_{org}}{\theta} = \frac{50kg/m^3}{20days} = 2.5kg/m^3.day$$

- Specific biogas production:
  - per reactor volume:

$$P = \frac{65m^3/d}{60m^3} = 1.08\frac{m^3/d}{m^3}$$

– per organic matter:

$$P = \frac{65m^3/day}{M_{org}\left[\frac{kg}{m^3}\right] \cdot \frac{V_{reactor}\left[m^3\right]}{\theta[days]}} = \frac{65}{50.\frac{60}{20}} = 0.43\frac{m^3}{kg_{org.matter}}$$

#### **Digestor reactor temperature**

Enzyme					Optimal	T rar	nge
'Psychrophilic'				20°C			
'Mesophilic'					20-45°C		
'Thermophilic'				>45°C			
relative CH₄ production		.00%				heat	any reactors operate at 28-37°C () they are red by burning t of the biogas
	10	20 3	30	40	50	60	°C

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ME460 Biogas

#### **Experience** values

- The determining factors in biogas production are:
  - temperature; part of the biogas is used to heat the reactor; the biogas production rate saturates at 40°C
  - residence time (days); saturates at 20 days
  - organic matter charge (usually 3-10%)

Production	Unit	Cows	Pigs
per animal and day	$m_{biogas}^3$ head day	1.3 <u>+</u> 0.3	1.5 <u>+</u> 0.6
per mass	$m_{biogas}^{3}/kg_{org.matter}$	0.3 <u>+</u> 0.05	0.5 <u>+</u> 0.05

 $\rightarrow$ 1.5 m<sup>3</sup>/day @ 20 MJ/m<sup>3</sup> = 30 MJ/day  $\approx$  8 kWh/day

= equivalent to 2  $m^2$  of thermal solar collectors

Any farm animal produces ca. 18-20 kg of manure per year per kg of its own body weight

### **Biogas vs. natural gas**

Property	Unit	NG	BG (60% CH <sub>4</sub> )
LHV	MJ / m <sup>3</sup>	36	21.5
Density	kg/m <sup>3</sup>	0.82	1.21
Ignition T	°C	620	700
Ignition speed in air	m/s	39	0.25
Air factor	-	9.5	5.7
Exhaust, max CO <sub>2</sub>	Vol%	11.9	17.8
Exhaust, dew point	°C	59	60-160

## Some characteristics of biogas production

- the digestate is a good quality **fertilizer** (2% nitrogen)
  - better than (air-)composted waste (<1% nitrogen)</li>
- a significant part of the produced biogas is used for **heating** of the digester and the installation itself (farm,...)
- (cold) desulfurisation of the biogas is done with FeCl<sub>3</sub> solution (to precipitate FeS); sulfur is removed as it is poisonous (for the atmosphere but also in downstream CHP engines or fuel cells)

# **Biogas use and potential (EU)**

	2007	gas engines 介	ultimate
Source	Use (PJ)	kW <sub>e</sub> /site	Potential
Effluents	7	200 kW	140 PJ
Sewage	37	50-200	215
Manure	30	10-100	750
Solid agro	45		1370
MSW,ISW	15	0.1-1 MW	330
Landfill	120	1 MW	-
TOTAL	254 PJ	huge margin	2805 PJ
	(6 Mtoe)		(67 Mtoe)

### **Biogas application examples (CH)**

Source	Biogas m³/day	% CH <sub>4</sub>	% yr Ioad	Installed power	Effi- ciency
Farm 37 cattle	70	57	60	5 kW <sub>el</sub>	18%
Sewage 30'000 p.	1000	65	65	130 kW <sub>el</sub>	28%
MSW 80'000 p.	1300	60	95	90 kW <sub>el</sub>	25%

=> small power sites (gas engines); low (electrical) efficiency

## Special case of landfill gas (LFG)

- (multi) $MW_{el}$ -size sites (with gas engines, gas turbines)
- an important fraction of world biogas (20 Mtoe)
- 3 Mtoe in EU-27
- important anthropogenic GHG emitter! (as CH<sub>4</sub>)
- often heavily contaminated (with F, CI, NH<sub>3</sub>, H<sub>2</sub>S, Si,...)
- often of low calorific value (diluted with  $N_2/O_2$ )
  - engines stop running <45% CH<sub>4</sub>
  - fuel-assisted flaring or venting !