Renewable Energy

- Outline:
 - Conversion pathways solar-to-fuel
 - Hybrid pathways
 - Solar thermochemistry
 - Photochemistry



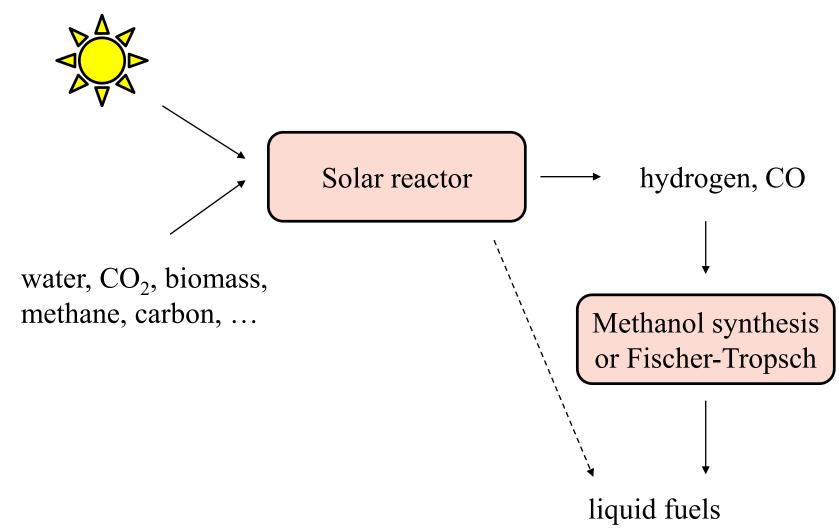
Learning outcomes of todays lecture

• Solar fuels:

- How can solar energy be converted into fuels?
- What is a hybrid pathway?
- Why using fossil fuels together with solar energy?
- What is solar thermochemistry and how can it be used for solar fuel processing?
- Why is solar water-splitting via multi-step water splitting cycles preferred compared to direct thermolysis?
- What is photoelectrochemistry and how can it be used for solar fuel processing?
- What other chemical commodities or materials can be processed using solar energy?

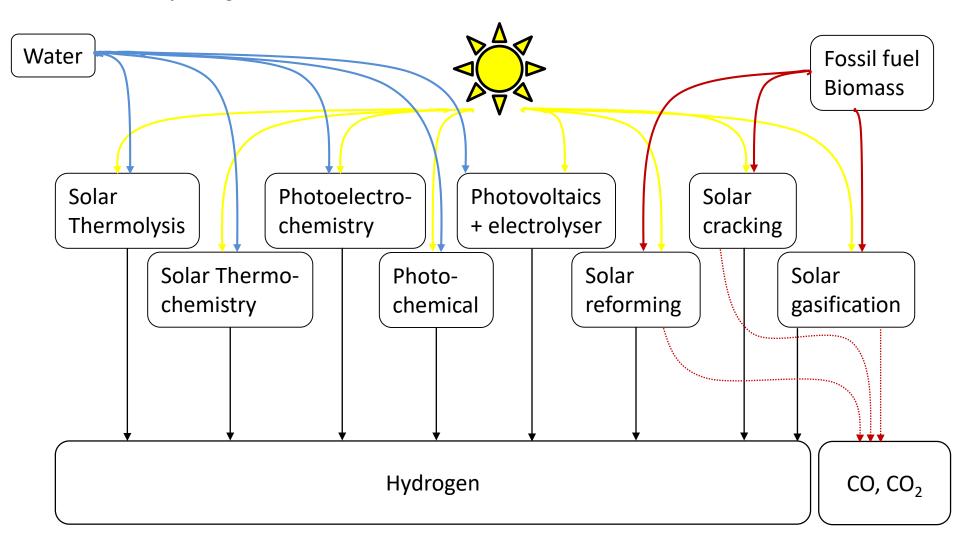


• Solar to fuels:



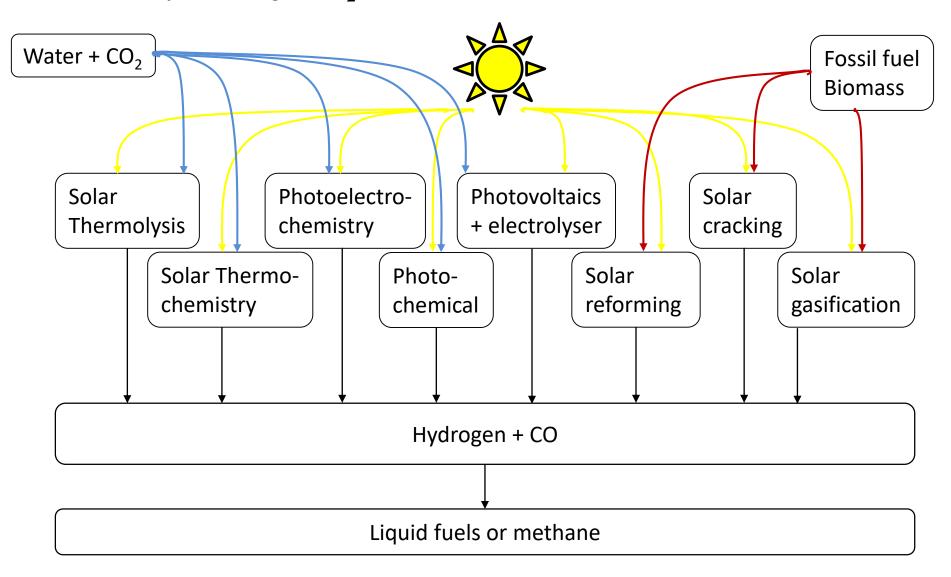


• Solar to hydrogen:





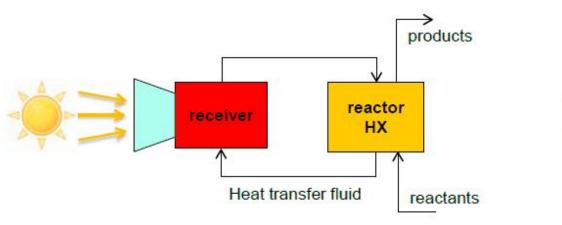
• Solar to synthesis gas (H_2+CO) :





- General considerations:
 - What solar radiation concentration technology can be used (if needed)?
 - What solar reactor can be used and what are the requirements?
 - How can the sun be coupled into the process?
 - What can the reactor look like?
- Reactor concepts:

Decoupled receiver+reactor
Possibly with high-temperature storage

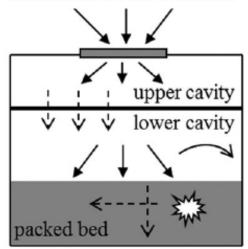




• Reactor concepts:

indirectly irradiated packed-bed

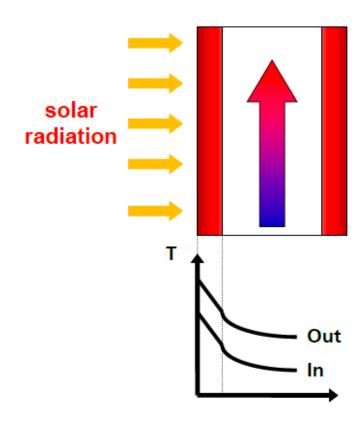
concentrated solar radiation





• Reactor concepts:

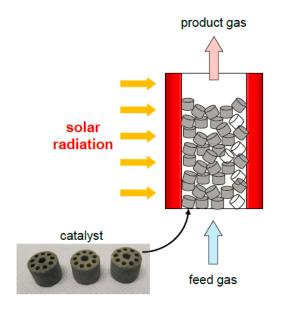
Tube receiver

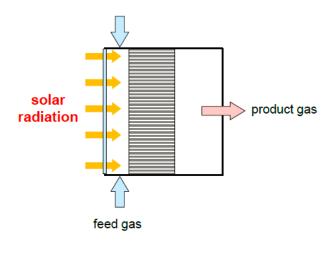


Also: open versus closed systems



- Reactor concepts:
 - Stationary



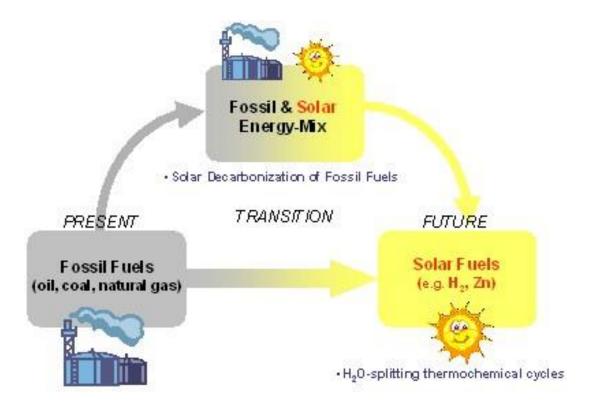


absorber coated with functional materials to catalyze reaction

- Moving:
 - Fluidized particle bed
 - Falling particle film
 - Rotating kiln
 - Moving particle bed



• In the transition to a renewable future, hybrid pathways using fossil fuels exclusively as chemical source for the fuel production and solar energy as the process heat



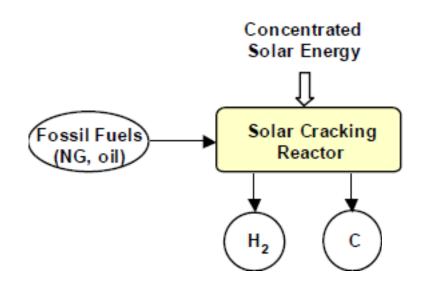


• Thermal cracking: complex organic molecules such as heavy hydrocarbons are broken down into simpler molecules such as light hydrocarbons, by the breaking of carbon-carbon bonds in the precursors at high temperatures and by using catalysts

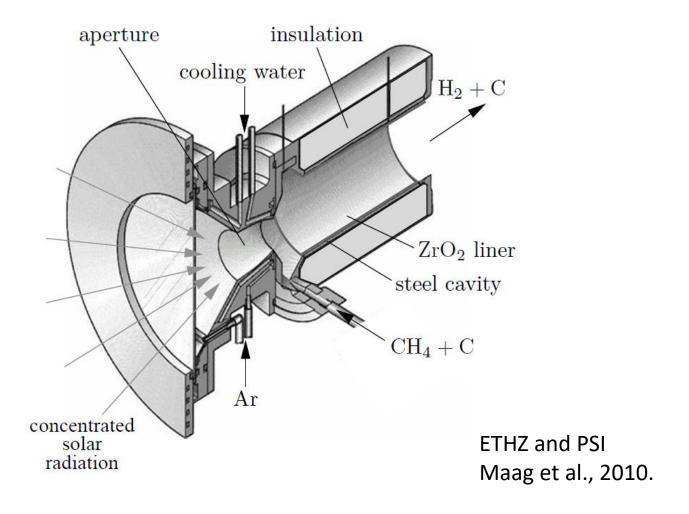
$$CH_4 \rightarrow C + 2H_2 (\Delta H = 74.85 \text{ kJ/mol})$$

• General:

$$C_n H_m \rightarrow nC + (m/2)H_2$$

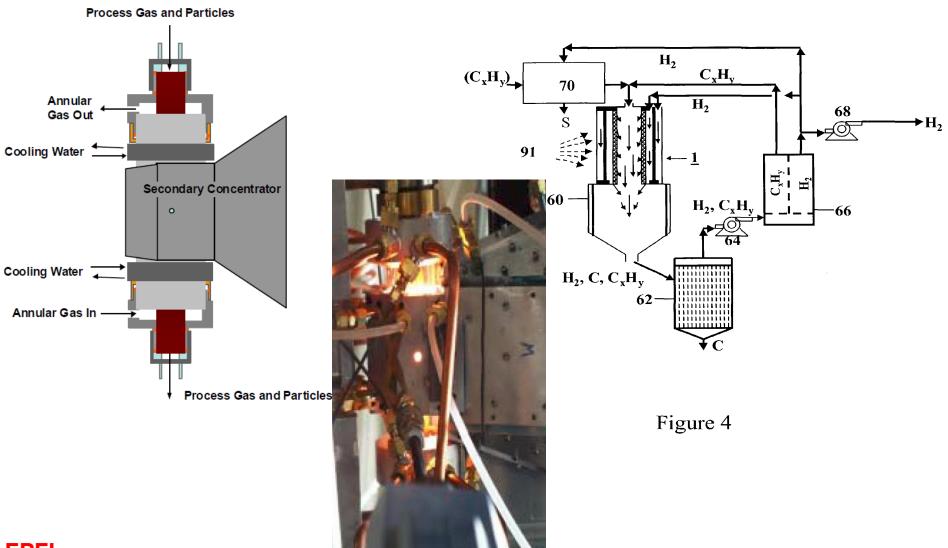


• Solar reactors developed for thermal cracking:





Solar reactors developed for thermal cracking: CU Boulder
 Dahl and Weimer et al., 2004.



Sulfur

Steam

• Steam reforming: uses light hydrocarbon feedstock, usually methane, reacts it at elevated temperatures with steam and catalytically converts the feed into hydrogen

$$CH_4 + H_2O \rightarrow CO + 3H_2 \ (\Delta H = 206 \text{ kJ/mol})$$

- Operates around 700 925°C
- Can achieve 65 75% efficiency

water gas shift: CO + H_2O -> CO_2 + H_2 (ΔH = -41 kJ/mol)



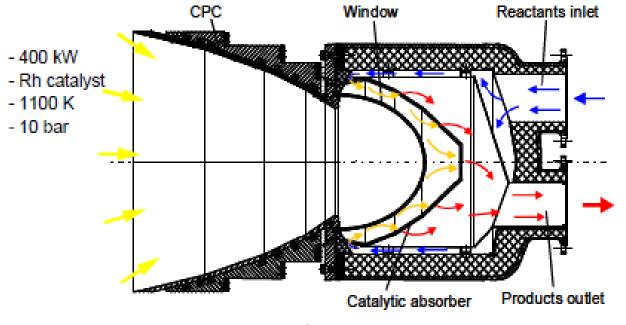
Heat recovery

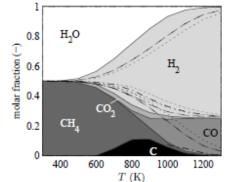
Shift Reaction

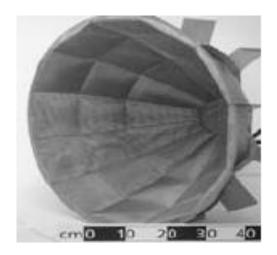
Separation

• Solar reactors developed for steam reforming Solar gasification of methane $(CH_4 + H_2O \rightarrow CO + 3H_2)$, DLR

SOLREF project









- **Gasification**: uses carbonaceous materials, reacts it at high temperatures (>700 °C), without combustion, with a controlled amount of steam, oxygen, and/or CO₂. Results in CO, H₂, and CO₂.
- E.g. for coal, or C-sources

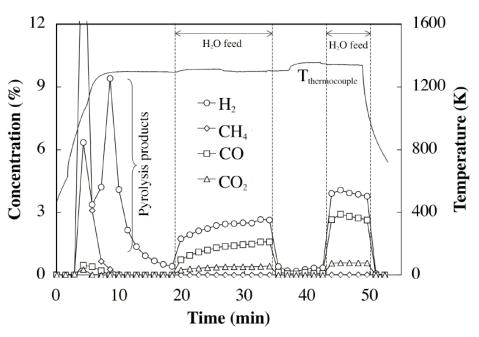
$$C + H_2O \rightarrow CO + H_2$$

• More realistic (especially for biomass, or C-waste):

$$CH_xO_yS_zN_u + (1-y)H_2O = \frac{1}{2}(x+2(1-y)-2z)H_2 + CO + zH_2S + \frac{1}{2}uN_2$$



- Consists of (sequential or simultaneous):
 - Dehydration
 - Pyrolysis (thermal decomposition in the absence of O₂, devolatilization)
 - Gasification (heterogeneous gas-soild reaction of pyrolysis residue with reactive gas)
 - Combustion
 - Water-gas-shift

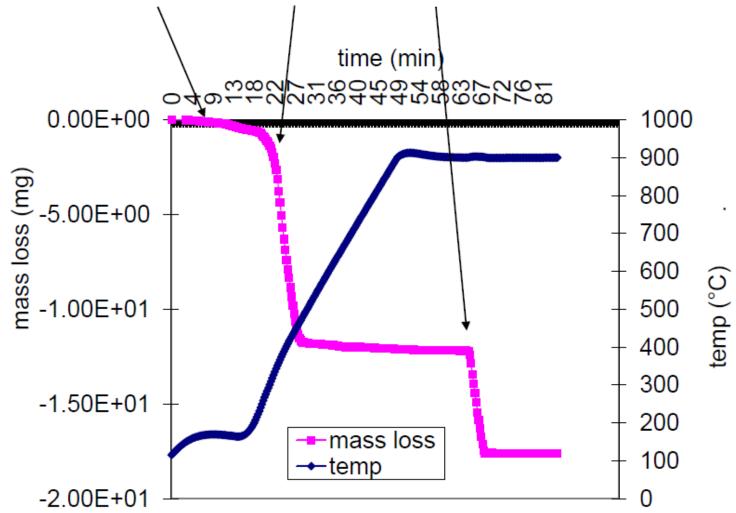


Trommer, Diss ETH, 2006.



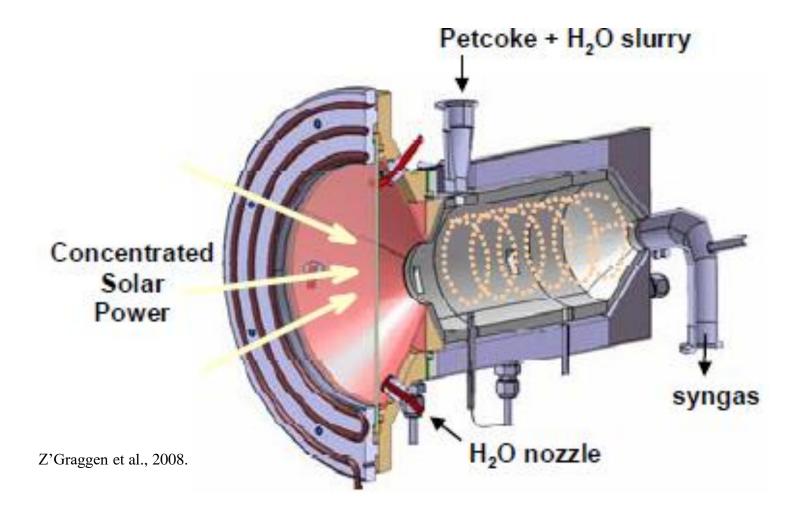
• Gasification (thermographimetric experiment):

Dehydration, Pyrolysis, Gasification



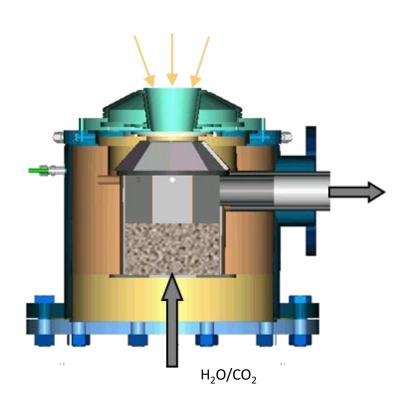


- Solar reactors developed for gasification:
 - Steam gasification of petcoke, ETH





- Solar reactors developed for gasification:
 - Steam gasification of carbonaceous waste material (ETH, PSI)





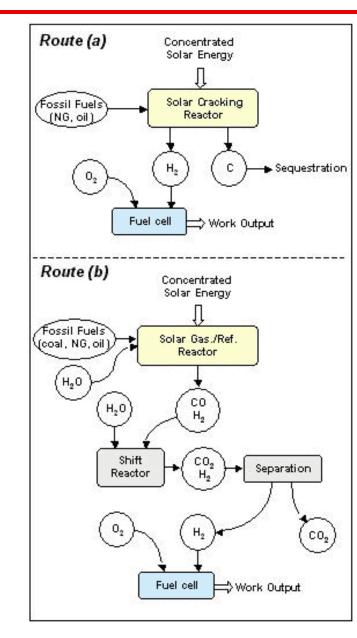
Piatkowski et al., 2010.



- Hydrogen derived from fossil fuels has many impurities:
 - From combustion: CO₂, CO, N₂
 - From the feedstock: sulfur
- Purification:
 - Desulfurization for gaseous feedstock: calcium-based slurries (SO₂ to sulfites and sulfates)
 - Desulfurization from solid/liquid feedstock: via catalysts into H₂S
 - CO₂ removal:
 - temperature swing adsorption (solubility variation of CO₂ with temperature)
 - pressure swing adsorption (pressure dependent absorption of e.g. zeolites)
 - special membranes (cellulose)
 - CO removal from H₂ mixture: Hydrogen-permeable membranes made of metals (palladium)



- Hybrid solar conversion
 - Advantage of hybrid process vs.
 conventional autothermal processes:
 - the gaseous products are not contaminated by combustion's by-products
 - the discharge of pollutants to the environment is reduced
 - the calorific value of the feedstock is upgraded
 - the fuel is decarbonized
 - there is no need for energy-intensive processing of pure oxygen





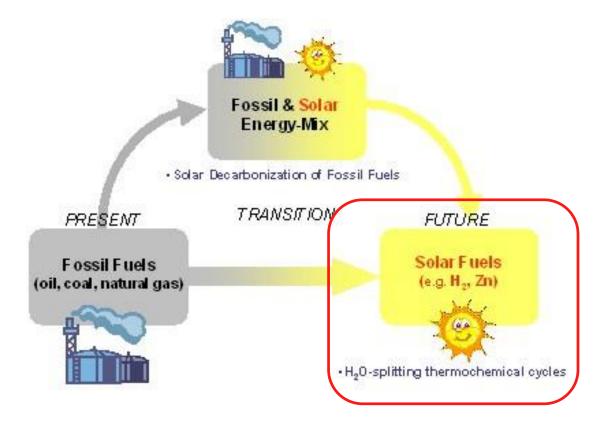
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Solar thermolysis and thermochemistry

• In the transition to a renewable future, hybrid pathways using fossil fuels exclusively as chemical source for the fuel production and solar energy as the process heat

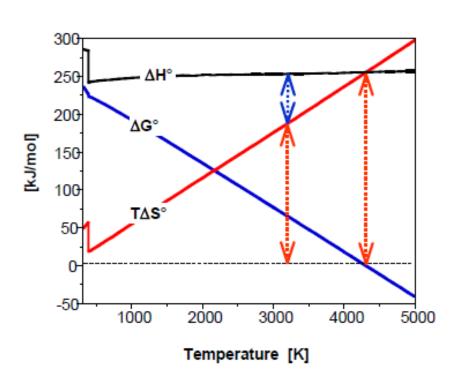


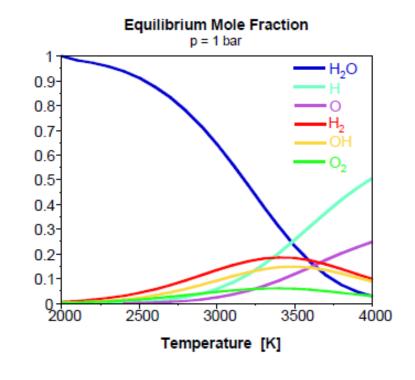


Solar thermolysis

• Solar thermolysis

- Solar energy is used as process heat of chemical reaction
- Direct thermolysis of water: $H_2O \rightarrow 1/2O_2 + H_2$

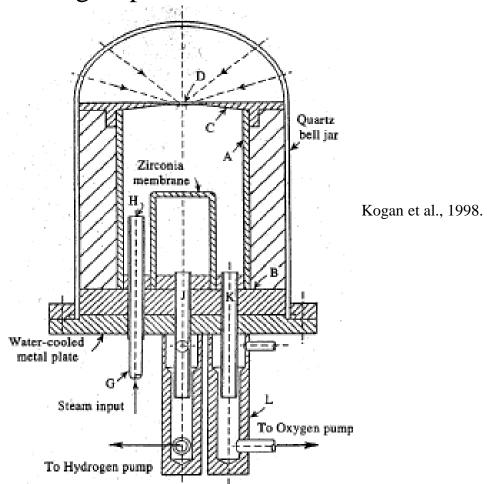






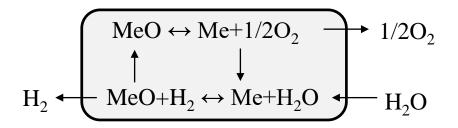
Solar thermolysis

- Reactor concept for solar thermolysis
 - Product separation by:
 - High temperature membranes
 - Rapid quenching of products





- Solar thermochemical cycles
 - Solar energy is used as process heat of chemical reaction
 - Multi-step water-splitting reactions:



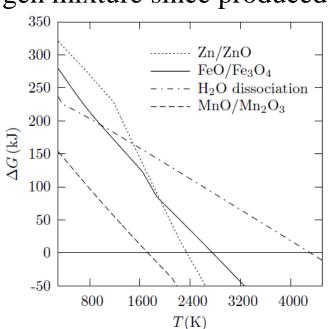
Omit explosive hydrogen and oxygen mixture since produced in

separate steps

Requires lower temperatures

Possible redox pairs (Me/MeO):

- Fe₂O₄/FeO
- Ce₂O₃/CeO₂,
- ZnO/Zn
- $SnO/SnO_2 \dots$

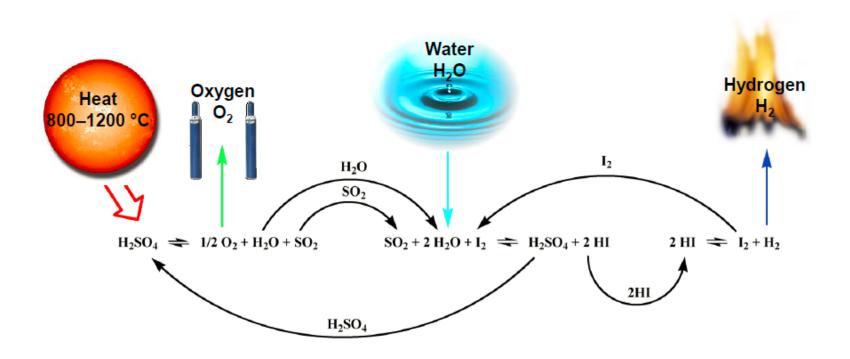




• Possible redox pairs for two-step cycles:

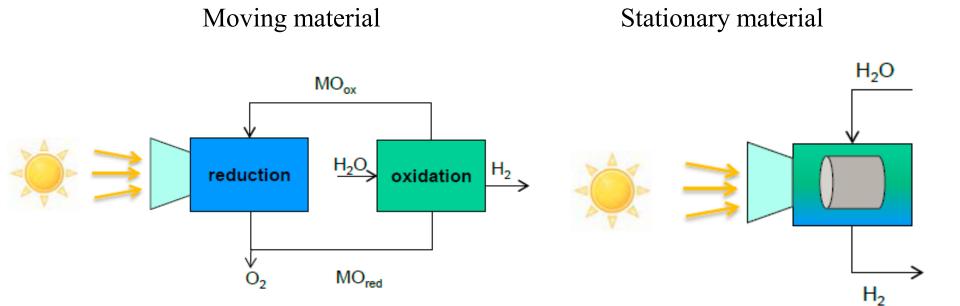
Cycle	Reactions	Cycle	Reactions
Zn/ZnO	$ZnO \rightarrow Zn + O_2$	SoO ₂ /SiO	$SiO_2 \rightarrow SiO + 1/2 O_2$
	$Zn + H_2O \rightarrow ZnO + H_2$		$SiO+H_2O\rightarrow SiO_2+H_2$
Fe ₃ O ₄ /FeO	$Fe_3O_4 \rightarrow 3 FeO + \frac{1}{2}O_2$	W/WO_3	$WO_3 \rightarrow W+3/2 O_2$
	$3 \text{ FeO} + \text{H}_2\text{O} \rightarrow \text{Fe}_3\text{O}_4 + \text{H}_2$		$W+3H_2O\rightarrow WO_3+3H_2$
In_2O_3/In_2O	$In_2O_3 \rightarrow In_2O+1/2 O_2$	Hg/HgO	$Hg+H_2O\rightarrow HgO+H_2$
	$In_2O+2H_2O\rightarrow In_2O_3+2H_2$		$HgO\rightarrow Hg+1/2O_2$
SnO ₂ /Sn	$SnO_2 \rightarrow Sn+O_2$	Cd/CdO	$Cd+H_2O\rightarrow CdO+H_2$
	$Sn+2H_2O \rightarrow SnO2+2H_2$		$CdO \rightarrow Cd+1/2O_2$
MnO/MnSO ₄	$MnSO_4 \rightarrow MnO + SO_2 + 1/2O_2$	CO/CO ₂	$CO+H_2O\rightarrow CO_2+H_2$
	$MnO+H_2O+SO_2\rightarrow MnSO_4+H_2$		$CO_2 \rightarrow CO + 1/2O_2$
FeO/FeSo ₄	$FeSO_4 \rightarrow FeO + SO_2 + 1/2O_2$	Ce_2O_3/CeO_2	$CeO_2 \rightarrow Ce_2O_3$
	$FeO+H_2O+SO_2 \rightarrow FeSO_4+H_2$		$Ce_2O_3+H_2O\rightarrow 2CeO_2+H_2$
CoO/CoSO ₄	$CoSO_4 \rightarrow CoO + SO_2 + 1/2O_2$	Mg/MgO	$MgO \rightarrow Mg+1/2O_2$
	$CoO+H_2O+SO_2\rightarrow CoSO_4+H_2$		$Mg+H_2O\rightarrow MgO+H_2$
Fe ₃ O ₄ /FeCl ₂	$Fe_3O_4+6HCl\rightarrow 3FeCl_2+3H_2O+1/2O_2$	SnO/SnO2	$SnO_2 \rightarrow SnO + 1/2O_2$
	$3\text{FeCl}_2+4\text{H}_2\text{O}\rightarrow\text{Fe}_3\text{O}_4+6\text{HCl}+\text{H}_2$		$SnO+H_2O\rightarrow SnO_2+H_2$
Mo/Mo ₂	$MoO_2 \rightarrow Mo + O_2$		
	$Mo+2H_2O\rightarrow MoO_2+2H_2$		
CDCI			

- Three-step water-splitting cycles, e.g. sulfur-iodine:
 - further lower temperatures
 - but run in corrosive environment





• Reactor concepts: two-step cycles

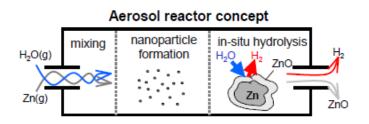




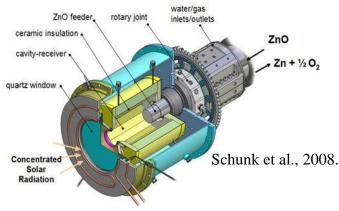
- Zn/ZnO-based proposed reactors, e.g. at ETH Zürich and PSI:
 - High-temperature reactor
 - 10 kW reactor
 - Reactor temperature: 2000 K
 - Peak concentration: 5800 suns



- Reactor temperature: 1263 K







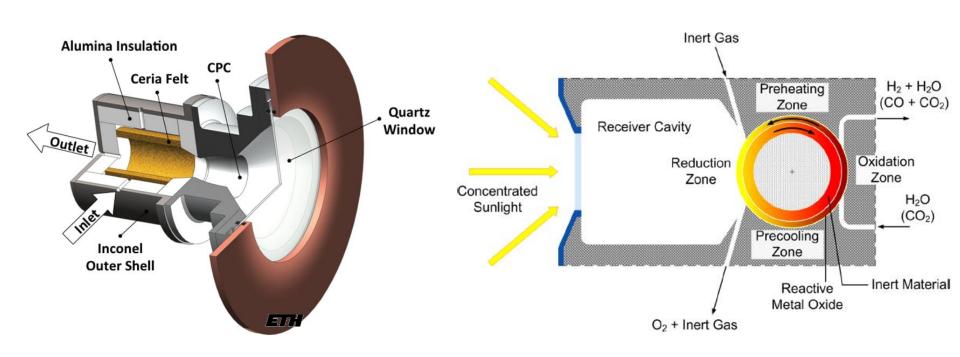
Melchior et al., 2009.



Ceria-based proposed reactors, e.g.:

ETH Zürich

University of Minnesota

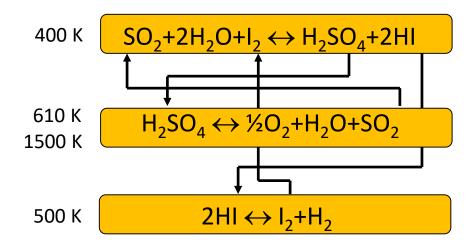


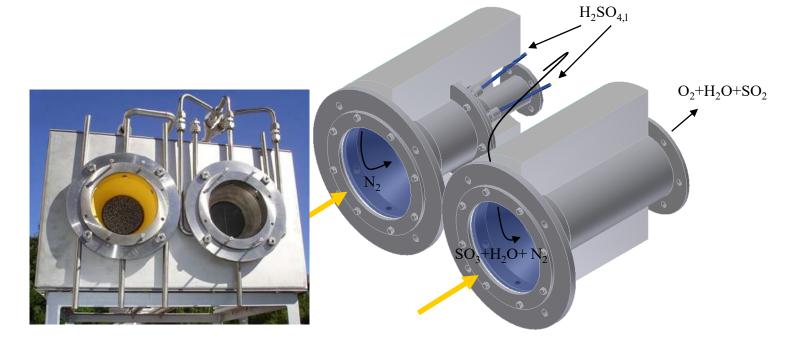
Temperature in reduction reaction: ~ 1800 K

Temperature in oxidation reaction: ~ 1200 K



• SI-cycle, DLR Germany







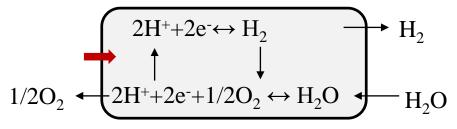
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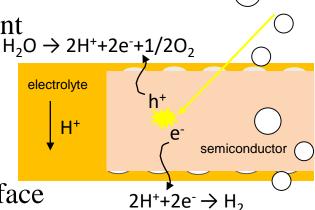


Photoelectrochemistry

- Photoelectrochemical processes
 - Solar energy is used as photon energy for the internal production of charge, which is separated at the solid-liquid junction
 - Multi-step water-splitting reactions (E_0 =1.23 V):

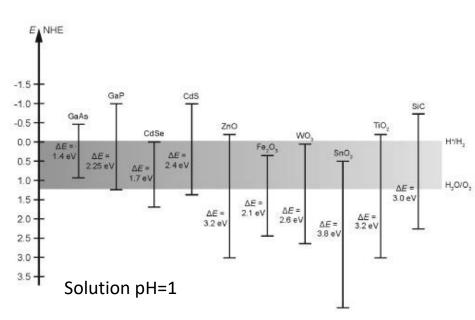


- Works at room temperature
- Spectral distribution of solar radiation important
- Processes:
 - Solar absorption
 - Electron-hole generation
 - Use electron and holes at liquid-solid interface
 - Ionic transport



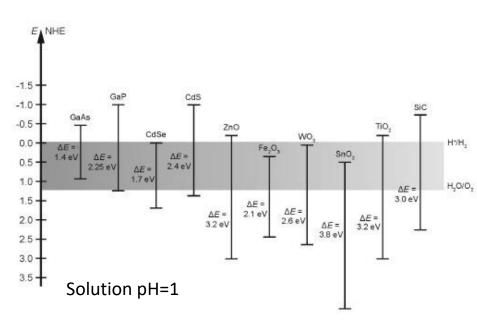
Photoelectrochemistry

- Stringent material requirements:
 - band gap size
 - suitable band edge position
 - high chemical stability in the dark and under illumination, as well as under highly acidic or base conditions
 - efficient charge transport in the semiconductor
 - selective and efficient electrochemical reactions
 - earth-abundance and low costs





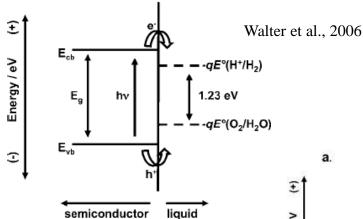
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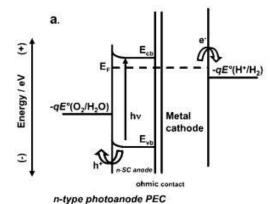


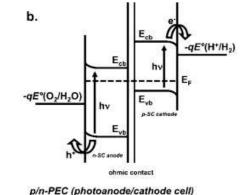
• Band gap and band position of photoelectrode material must match reaction potentials:

Energy / eV



• Various possible architectures:



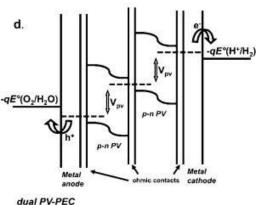


C.

E_{cb}

V_{pv}

P-n PV



EPFL

n-type photoanode/PV - PEC

KE, Haussener | Mai, 2021

• Calculations:

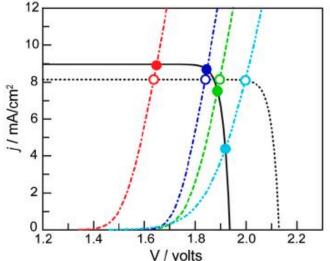
 Photoactive material(s) will show diode-like current-potential behavior:

$$i = i_L - i_0 \left(\exp\left(\frac{qV}{kT}\right) - 1 \right)$$

- Electrochemical system shows losses:
 - Reaction overpotentials
 - Ohmic losses

$$E = E_0 + \eta_{\rm a} + \eta_{\rm c} + iR_{\rm sol} + E_{\rm mem} + E_{\rm conc} > E_0$$

- Concentration losses
- Electrochemical load curve will show electrolyzer like load curve
- Intersection between both is operating point



Surendranath et al., 2012



- Calculations:
 - Electrochemical system shows losses:
 - Reaction overpotentials
 - E.g. via Tafel equations:

$$\eta_{\rm a} = a_1 \log \left(\frac{i}{i_{0\rm a}}\right)$$

Tafel slope $\eta_{\rm a} = a_1 \log \left(\frac{i}{i_{\rm 0a}}\right)$ $\eta_{\rm c} = a_2 \log \left(\frac{i}{i_{\rm 0a}}\right)$

– Or Buttler-Volmer:

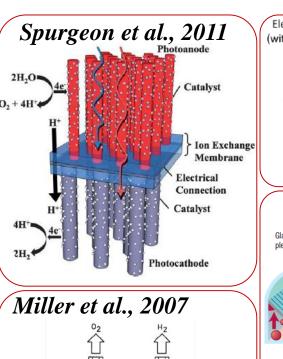
Exchange current density

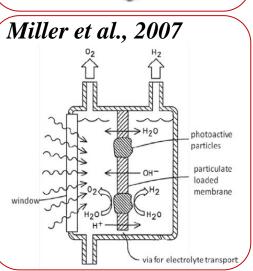
$$i_{\rm R} = i_{\rm 0a/c} \left[\exp \left(\frac{\alpha_{\rm a} F \left(\Phi_{\rm s} - \Phi_{\rm 1} - E_{\rm 0} \right)}{RT} \right) - \exp \left(\frac{\alpha_{\rm c} F \left(\Phi_{\rm s} - \Phi_{\rm 1} - E_{\rm 0} \right)}{RT} \right) \right]$$

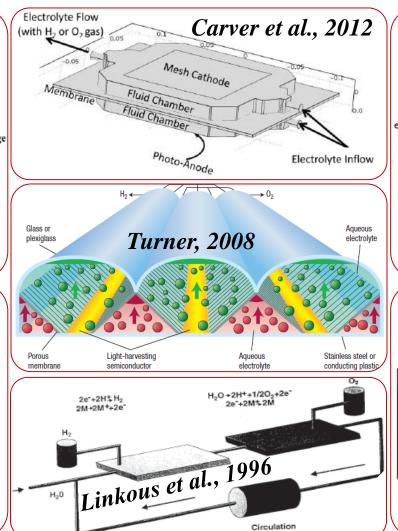
Ohmic losses account for resistances in electrolyte, membrane, and solid conductor: Characteristic ion and electron path length

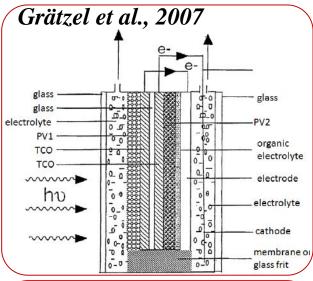
$$\Delta V_{\text{ohm}} = i \rho_{\text{sol}} l$$
resistivity

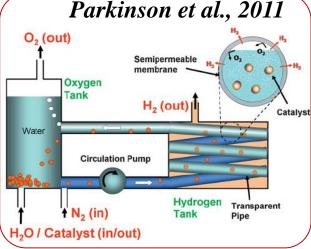
Proposed devices





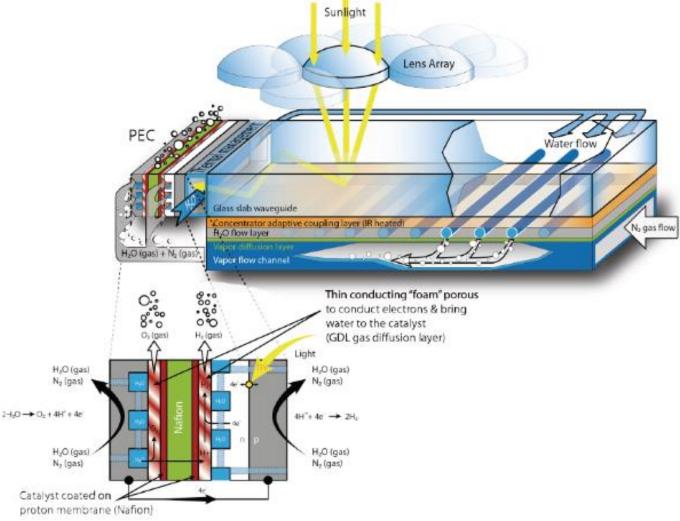




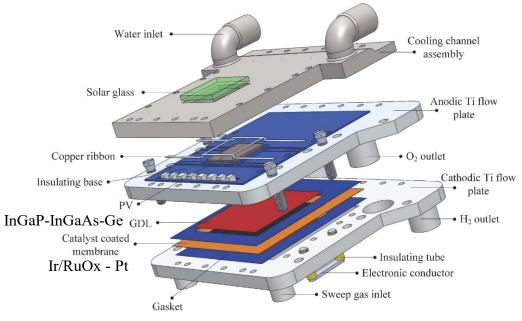


Proposed devices

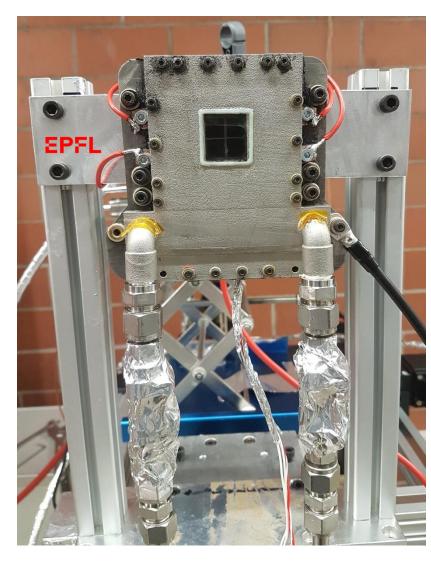




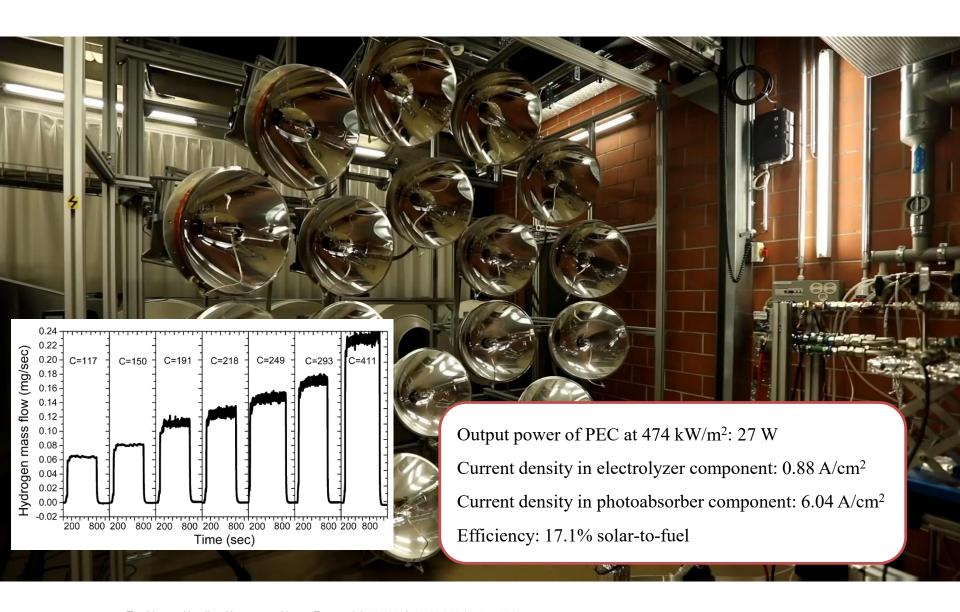








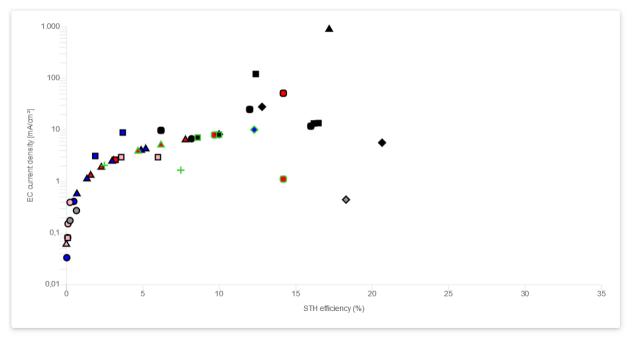
Experimental demonstration





Photoelectrochemistry - Comparison

Community outreach: dynamic and online: – http://specdc.epfl.ch/



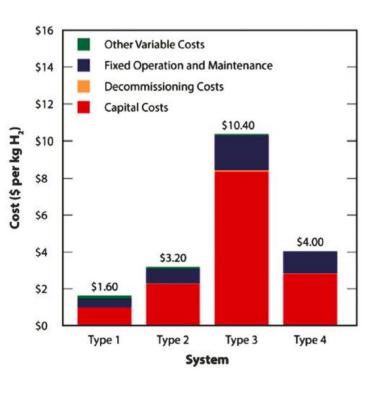
w/o multi-module demonstrations w/o multiple electrolyzer demonstrations

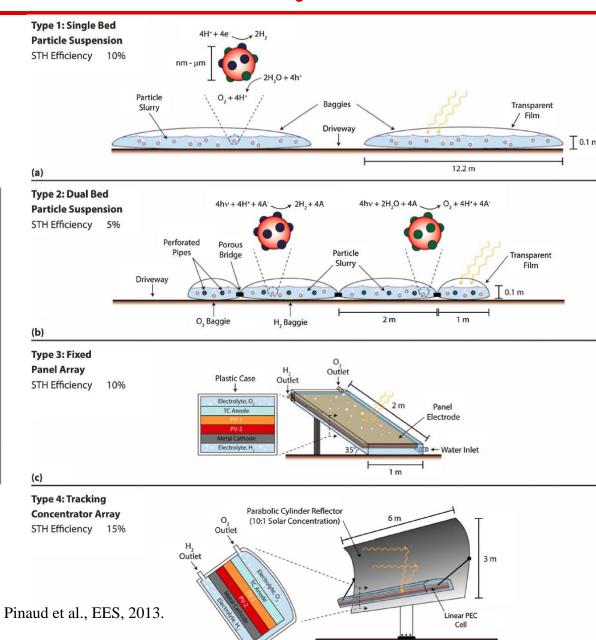
LEGEND					
Fill color - PV / photoabsorber material	Boundary color - EC material	Symbol shape - PV / photoabsorber and EC configuration			
All III-V	Rare metal-based (expensive)	0	2J, integrated PVs and catalyst	+	3J, integrated PVs and catalyst
Partial III-V	Abundant (cheap)		2J, integrated PVs, wired catalyst	Δ	3J, integrated PVs, wired catalyst
All Si		♦	2J, non-integrated PVs or catalyst	0	3J, non-integrated PVs or catalyst
Partial Si					
Oxides and others					

Tembhurne, Nandjou, Haussener, Nature Energy, doi: 10.1038/s41560-019-0373-7, 2019



Proposed devices



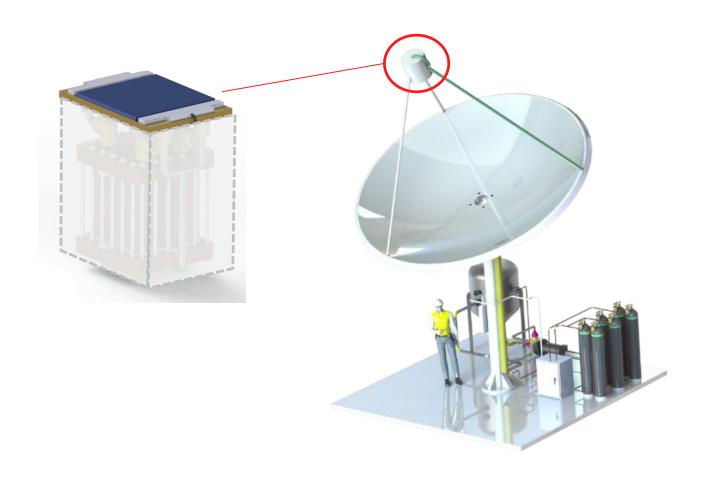


Water Inlet-

(d)



Scaling – ongoing @LRESE



kW-scale, long-term, on-sun demonstration, 0.5 kg of hydrogen per day

Scaling – ongoing @LRESE



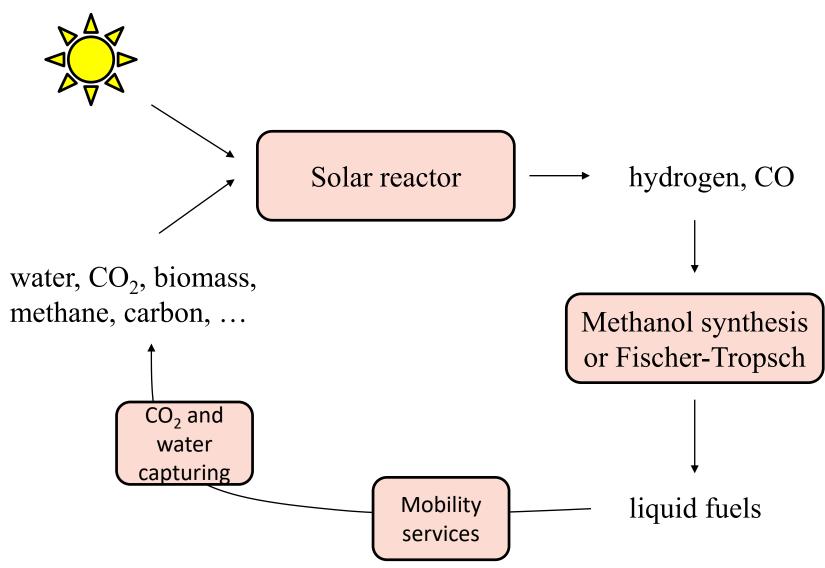
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Sustainability issue

• Solar to fuels:





Solar materials

- Solar to materials:
 - In principle any other chemical reaction could be driven by solar thermochemistry or photoelectrochemistry if enthalpy of reaction matches solar irradiation, or equilibrium potential and band edge position matches solar irradiation and material combinations

− E.g.:

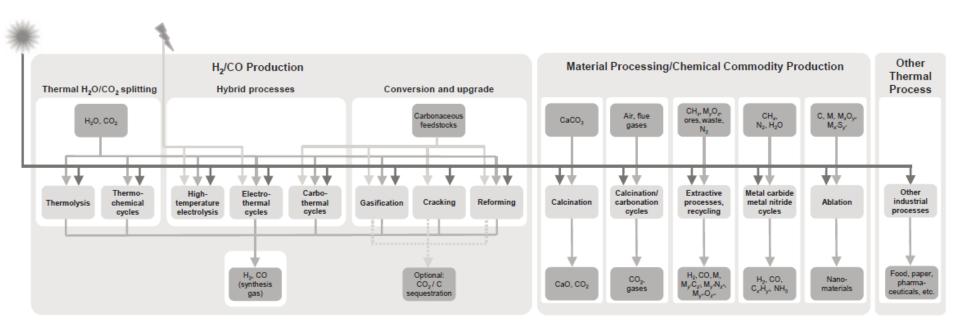
Carbothermic reduction of alumina under near vacuum conditions

• Ammonia production $\begin{array}{c} \text{Concentrated Solar Energy} \\ \text{Solar REACTOR} \\ \text{Nitrogen} \\ \text{Nitrogen} \\ \text{Water} \\ \\ \text{Water} \\ \\ \text{Precycle} \\ \text{Alp } O_3 + 3C + N_2 \rightarrow 2\text{AIN} + CO \\ \text{Alg } O_3 + 3C + N_2 \rightarrow 2\text{AIN} + 6H_2 + 3CO} \\ \text{Almonia} \\ \text{Syngas} \\ \text{Ammonia} \\ \text{Syngas} \\ \text{Syngas} \\ \text{Alp } O_3 \\ \text{Alp } O_3$



Solar materials

• Thermochemical:



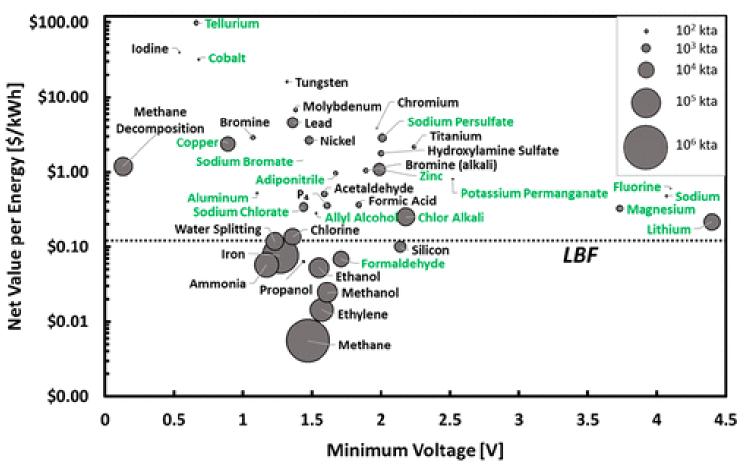
Bader et al., 2016



Solar materials

• (Photo)electrochemical:

Absolute Maximum Value per Energy Input vs Minimum Voltage Required



Maximum net value per energy input (log scale) plotted versus minimum voltage required for all electrochemical processes or electrochemical equivalents of thermochemical processes. For each point, the width of the circle corresponds to the relative market size. Processes highlighted in green are conducted electrochemically in industry, to any appreciable extent. The lower bound of feasibility (LBF) is plotted as the horizontal dashed line

Palmer et al., Technoeconomics of Commodity Chemical Production Using Sunlight, ACS Sustainable Chemistry & Engineering, 2018



Learning outcomes of todays lecture

• Solar fuels:

- How can solar energy be converted into fuels?
- What is a hybrid pathway?
- Why using fossil fuels together with solar energy?
- What is solar thermochemistry and how can it be used for solar fuel processing?
- Why is solar water-splitting via multi-step water splitting cycles preferred compared to direct thermolysis?
- What is photoelectrochemistry and how can it be used for solar fuel processing?
- What other chemical commodities or materials can be processed using solar energy?



Solar energy conversion systems

• Literature

- Review articles:
 - Meier et al., Solar thermochemical production of fuels, Advances in Science and Technology, vol. 74, pp. 303-312, 2010.
 - Lipinski et al., Review of heat transfer research for solar thermochemical applications, Journal of Thermal Science and Engineering Applications, 5: 021005, 2013.
 - Walter et al., Solar water splitting cells, Chemical Reviews, vol. 110, pp. 6446–6473, 2010.

