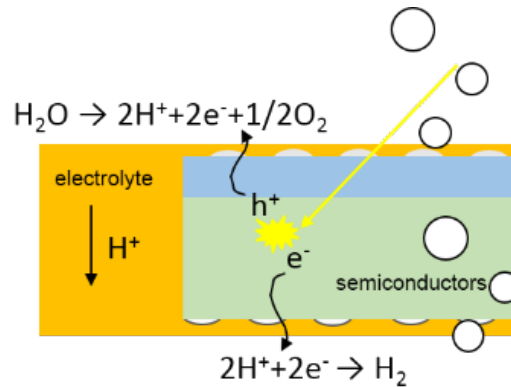


## Renewable Energy: Solar Fuels Exercise

This exercise deals with assessment of solar fuels generation. In the first part, the production of hydrogen by photoelectrochemical water-splitting is investigated. In the second part, you use solar thermochemical route for the production of synthesis gas used in a fuel cell.

1. The schematic of a photoelectrochemical cell is shown in figure 1.

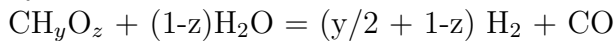


**Figure 1:** Schematic of the photoelectrochemical water splitting device

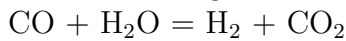
- (a) The photoabsorber is a dual absorber made of  $Si$  (band gap 1.1 eV) and  $BiVO_4$  (band gap 2.16 eV). Which of the two cells ( $Si$  or  $BiVO_4$ ) will you put on top of your device?
- (b) Calculate the fraction of incident light which is ideally absorbed in both cells.
- (c) Assume that the resulting cell performance can be calculated by
- $$i = i_0 - i_1 \cdot \left( e^{\frac{qV}{nk_B T}} - 1 \right)$$
- with  $i_0 = 115 \text{ A/m}^2, i_1 = 3 \cdot 10^{-42} \text{ A/m}^2, n = 1, T = 300 \text{ K}$   
 Determine the short circuit current and open circuit voltage. What is the fill factor of this dual absorber cell?
- (d) Assume that the load curve of the integrated electrochemical cell can be calculated by
- $$V = V_0 + i\rho l_p + a_1 \log\left(\frac{i}{i_{0a}}\right) + a_2 \log\left(\frac{i}{i_{0c}}\right)$$
- with  $V_0 = 1.23 \text{ V}, \rho = 0.1 \text{ } \Omega\text{m}, l_p = 8 \text{ cm}, a_1 = 0.035 \text{ V/dec}, i_{0a} = 0.00001 \text{ A/m}^2, a_2 = 0.03 \text{ V/dec}, i_{0c} = 0.001 \text{ A/m}^2, T = 300 \text{ K}$   
 Describe the meaning of the four terms on the right hand side and calculate the overpotentials at a current density  $i = 200 \text{ A/m}^2$ .
- (e) Plot the two curves (i.e. for both PV an electrochemical cell) in a V-i-plot (x-axis: V, y-axis: i) and read the operating potential and current density. Is it operating at the maximum power point? How could we operate more close to the maximum power point?

- (f) What is the efficiency of the cell, assuming an irradiation of  $1000 \text{ W/m}^2$ ?
- (g) Calculate how much hydrogen is produced per year and area assuming a continuous operation at the operating point for 1900 hours (high heating value of  $\text{H}_2 = 141 \text{ MJ/kg}$ ).

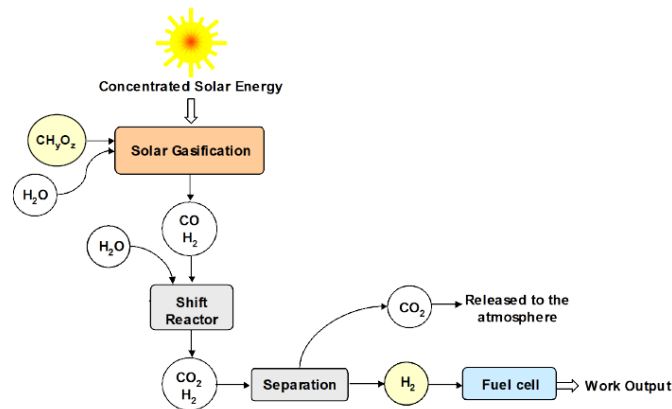
2. The solar steam-gasification of carbonaceous material for syngas production is represented by the net stoichiometric reaction:



Each mole of CO in the syngas is further water gas-shifted to generate an additional mole of  $\text{H}_2$  according to:



The  $\text{H}_2/\text{CO}_2$  mixture undergoes separation to  $\text{H}_2$  and  $\text{CO}_2$ .  $\text{H}_2$  produced is fed to a  $\text{H}_2/\text{O}_2$  fuel cell, while  $\text{CO}_2$  produced is released to the atmosphere. The process is schematically depicted in Fig. 2. The selected carbonaceous feedstock is wood, of elemental composition: 49 wt% C, 6 wt% H, and 45 wt% O.



**Figure 2:** Schematic representation of the solar gasification process for  $\text{H}_2$  generation

Assumptions:

- Solar reactor is a perfectly insulated blackbody cavity-receiver; only radiation losses are considered.
- Reactor operating temperature,  $T_{reactor} = 1200 \text{ K}$ .
- Mean solar flux concentration ratio,  $C = 1800 \text{ suns}$ .
- Normal beam insolation,  $I = 1 \text{ kW/m}^2$ .
- Mass flow rate of  $\text{CH}_y\text{O}_z$ ,  $\dot{n}_{\text{CH}_y\text{O}_z} = 1 \text{ mol/s}$ .

- The net power absorbed by the solar reactor matches the enthalpy change per unit time of the reaction  $\dot{Q}_{Reactor,net} = \dot{n}_{CH_yO_z} \cdot \Delta H = 210 \text{ kW}$ .
  - The water-gas shift reaction is carried out in an auto-thermal reactor.
  - The  $H_2/CO_2$  separation unit is based on the pressure swing adsorption technique (PSA) at 94% recovery rate.
  - The  $H_2/O_2$  fuel cell operates with a conversion efficiency of 62% of the high heating value of  $H_2$ .
  - Heating value of carbonaceous feedstock,  $HV_{CH_yO_z} = 570 \text{ kJ/mol}$ .
  - High heating value of  $H_2$ ,  $HV_{H_2} = 285 \text{ kJ/mol}$ .
- (a) Calculate  $y$  and  $z$  using the elemental composition of the carbonaceous feedstock. Calculate the number of moles of  $H_2$  and  $CO_2$  ideally produced for a mole of  $CH_yO_z$  gasified.
- Hint:  $\gamma_i = \frac{\nu_i/M_i}{\sum_n \nu_n/M_n}$ , with  $\gamma$  molar fraction,  $\nu$  weight fraction, and  $M$  molar mass of species  $i$ .
- (b) Calculate the absorption efficiency of the solar reactor,  $\eta_{absorption}$ .
- (c) Calculate solar power input,  $\dot{Q}_{solar}$ .
- (d) Calculate the electric power output of the  $H_2/O_2$  fuel cell,  $\dot{W}_{out}$ .
- (e) Calculate the Energy Gain Factor (EGF), defined as the ration of the electric output of the solar process to that obtained when using the same amount of C as a combustion fuel in a 40% efficient Rankine cycle.
- (f) Calculate the specific  $CO_2$  emissions, in units of  $kg \text{ CO}_2/kWh_e$ , for the solar process and for the 40% efficient Rankine cycle.