Renewable Energy

- Outline:
 - Conversion pathways solar-to-fuel
 - Hybrid pathways
 - Solar thermochemistry
 - Photochemistry

Learning outcomes of todays lecture

- Solar fuels:
 - How can solar energy be converted into fuels?
 - What is a hybrid pathway?
 - Why using fossil fuels together with solar energy?
 - What is solar thermochemistry and how can it be used for solar fuel processing?
 - Why is solar water-splitting via multi-step water splitting cycles preferred compared to direct thermolysis?
 - What is photoelectrochemistry and how can it be used for solar fuel processing?
 - What other chemical commodities or materials can be processed using solar energy?

• Solar to fuels:

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• Solar to hydrogen:



• Solar to synthesis gas (H₂+CO):



- General considerations:
 - What solar radiation concentration technology can be used (if needed)?
 - What solar reactor can be used and what are the requirements?
 - How can the sun be coupled into the process?
 - What can the reactor look like?
- Reactor concepts:

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Decoupled receiver+reactor Possibly with high-temperature storage Coupled receiver-reactor



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Reactor concepts:

indirectly irradiated packed-bed

directly irradiated vortex-flow

indirectly irradiated entrained flow







chemical reaction

• Reactor concepts:

Tube receiver



Volumetric receiver



• Also: open versus closed systems

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- Reactor concepts:
 - Stationary



– Moving:

- Fluidized particle bed
- Falling particle film
- Rotating kiln
- Moving particle bed

• In the transition to a renewable future, hybrid pathways using fossil fuels exclusively as chemical source for the fuel production and solar energy as the process heat



• **Thermal cracking**: complex organic molecules such as heavy hydrocarbons are broken down into simpler molecules such as light hydrocarbons, by the breaking of carbon-carbon bonds in the precursors at high temperatures and by using catalysts

$$CH_4 \rightarrow C + 2H_2 (\Delta H = 74.85 \text{ kJ/mol})$$

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• Solar reactors developed for thermal cracking:



• Solar reactors developed for thermal cracking: CU Boulder

Dahl and Weimer et al., 2004.



• **Steam reforming**: uses light hydrocarbon feedstock, usually methane, reacts it at elevated temperatures with steam and catalytically converts the feed into hydrogen

 $CH_4 + H_2O \rightarrow CO + 3H_2 (\Delta H = 206 \text{ kJ/mol})$

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• Solar reactors developed for steam reforming Solar gasification of methane ($CH_4 + H_2O \rightarrow CO + 3H_2$), DLR SOLREF project







- Gasification: uses carbonaceous materials, reacts it at high temperatures (>700 °C), without combustion, with a controlled amount of steam, oxygen, and/or CO₂. Results in CO, H₂, and CO₂.
- E.g. for coal, or C-sources

 $\mathrm{C} + \mathrm{H_2O} \rightarrow \mathrm{CO} + \mathrm{H_2}$

• More realistic (especially for biomass, or C-waste):

$$CH_xO_yS_zN_u + (1-y)H_2O = \frac{1}{2}(x+2(1-y)-2z)H_2 + CO + zH_2S + \frac{1}{2}uN_2$$

- Consists of (sequential or simultaneous):
 - Dehydration
 - Pyrolysis (thermal decomposition in the absence of O₂, devolatilization)
 - Gasification (heterogeneous gas-soild reaction of pyrolysis residue with reactive gas)
 - Combustion
 - Water-gas-shift



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• Gasification (thermographimetric experiment):



- Solar reactors developed for gasification:
 - Steam gasification of petcoke, ETH



- Solar reactors developed for gasification:
 - Steam gasification of carbonaceous waste material (ETH, PSI)





Piatkowski et al., 2010.

- Hydrogen derived from fossil fuels has many impurities:
 - From combustion: CO₂, CO, N₂
 - From the feedstock: sulfur
- Purification:
 - Desulfurization for gaseous feedstock: calcium-based slurries (SO₂ to sulfites and sulfates)
 - Desulfurization from solid/liquid feedstock: via catalysts into H_2S
 - CO₂ removal:
 - temperature swing adsorption (solubility variation of CO₂ with temperature)
 - pressure swing adsorption (pressure dependent absorption of e.g. zeolites)
 - special membranes (cellulose)
 - CO removal from H₂ mixture: Hydrogen-permeable membranes made of metals (palladium)

• Hybrid solar conversion

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- Advantage of hybrid process vs.
 conventional autothermal processes:
 - the gaseous products are not contaminated by combustion's by-products
 - the discharge of pollutants to the environment is reduced
 - the calorific value of the feedstock is upgraded
 - the fuel is decarbonized
 - there is no need for energy-intensive processing of pure oxygen



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Solar thermolysis and thermochemistry

• In the transition to a renewable future, hybrid pathways using fossil fuels exclusively as chemical source for the fuel production and solar energy as the process heat



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Solar thermolysis

- Solar thermolysis
 - Solar energy is used as process heat of chemical reaction
 - Direct thermolysis of water: $H_2O \rightarrow 1/2O_2 + H_2$



Solar thermolysis

- Reactor concept for solar thermolysis
 - Product separation by:
 - High temperature membranes
 - Rapid quenching of products



- Solar thermochemical cycles
 - Solar energy is used as process heat of chemical reaction
 - Multi-step water-splitting reactions:

$$H_{2} \leftarrow MeO \leftrightarrow Me+1/2O_{2} \rightarrow 1/2O_{2}$$

$$H_{2} \leftarrow MeO+H_{2} \leftrightarrow Me+H_{2}O \rightarrow H_{2}O$$

- Omit explosive hydrogen and oxygen mixture since produced in separate steps
- Requires lower temperatures
- Possible redox pairs (Me/MeO):
 - Fe₂O₄/FeO
 - Ce₂O₃/CeO₂,
 - ZnO/Zn
 - $SnO/SnO_2 \dots$



RE, Haussener | April, 2022 27/55

• Possible redox pairs for two-step cycles:

Cycle	Reactions	Cycle	Reactions
Zn/ZnO	$ZnO \rightarrow Zn + O_2$	SoO ₂ /SiO	$SiO_2 \rightarrow SiO + 1/2 O_2$
	$Zn + H_2O \rightarrow ZnO+H_2$		$SiO+H_2O \rightarrow SiO_2+H_2$
Fe ₃ O ₄ /FeO	$Fe_3O_4 \rightarrow 3 FeO + \frac{1}{2}O_2$	W/WO3	$WO_3 \rightarrow W+3/2 O_2$
	$3 \text{ FeO} + \text{H}_2\text{O} \rightarrow \text{Fe}_3\text{O}_4 + \text{H}_2$		$W+3H_2O \rightarrow WO_3+3H_2$
In ₂ O ₃ /In ₂ O	$In_2O_3 \rightarrow In_2O+1/2 O_2$	Hg/HgO	$Hg+H_2O\rightarrow HgO+H_2$
	$In_2O+2H_2O\rightarrow In_2O_3+2H_2$		$HgO \rightarrow Hg + 1/2O_2$
SnO ₂ /Sn	$SnO_2 \rightarrow Sn+O_2$	Cd/CdO	$Cd+H_2O\rightarrow CdO+H_2$
	$Sn+2H_2O \rightarrow SnO2+2H_2$		$CdO \rightarrow Cd+1/2O_2$
MnO/MnSO ₄	$MnSO_4 \rightarrow MnO+SO_2+1/2O_2$	CO/CO ₂	$CO+H_2O\rightarrow CO_2+H_2$
	$MnO+H_2O+SO_2\rightarrow MnSO_4+H_2$		$CO_2 \rightarrow CO + 1/2O_2$
FeO/FeSo ₄	$FeSO_4 \rightarrow FeO+SO_2+1/2O_2$	Ce ₂ O ₃ /CeO ₂	$CeO_2 \rightarrow Ce_2O_3$
	$FeO+H_2O+SO_2\rightarrow FeSO_4+H_2$		$Ce_2O_3+H_2O\rightarrow 2CeO_2+H_2$
CoO/CoSO4	$CoSO_4 \rightarrow CoO + SO_2 + 1/2O_2$	Mg/MgO	MgO \rightarrow Mg+1/2O ₂
	$CoO+H_2O+SO_2\rightarrow CoSO_4+H_2$		$Mg+H_2O\rightarrow MgO+H_2$
Fe ₃ O ₄ /FeCl ₂	$Fe_3O_4+6HCl \rightarrow 3FeCl_2+3H_2O+1/2O_2$	SnO/SnO2	$SnO_2 \rightarrow SnO+1/2O_2$
	$3FeCl_2+4H_2O \rightarrow Fe_3O_4+6HCl+H_2$		$SnO+H_2O\rightarrow SnO_2+H_2$
Mo/Mo ₂	$MoO_2 \rightarrow Mo+O_2$		
	$M_0+2H_2O \rightarrow M_0O_2+2H_2$		

- Three-step water-splitting cycles, e.g. sulfur-iodine:
 - further lower temperatures
 - but run in corrosive environment



• Reactor concepts: two-step cycles



- Zn/ZnO-based proposed reactors, e.g. at ETH Zürich and PSI:
 - High-temperature reactor
 - 10 kW reactor
 - Reactor temperature: 2000 K
 - Peak concentration: 5800 suns

- Hydrolysis reactor:
 - Reactor temperature: 1263 K







Melchior et al., 2009.

• Ceria-based proposed reactors, e.g.: ETH Zürich

University of Minnesota



Temperature in reduction reaction: ~ 1800 K Temperature in oxidation reaction: ~ 1200 K



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Photochemistry



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Water splitting



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Key steps in photo(electro)catalysis



1) Capture of light energy 2) Separation of photogenerated charge carriers

3) Surface catalysis

$$\Phi_{H_2} = \phi_{Abs.} \times \phi_{Sep.} \times \phi_{Cat.}$$

Semiconductors

- Stringent material requirements:
 - band gap size

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- suitable band edge position
- high chemical stability in the dark and under illumination, as well as under highly acidic or base conditions
- efficient charge transport in the semiconductor
- selective and efficient electrochemical reactions
- earth-abundance and low costs



Strategies to improve activity



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 \checkmark

 \checkmark

 \checkmark

 \checkmark

 \checkmark

A new member of 2D carbon allotropes composed of *sp-sp*² carbon atoms.



Graphyne Family:





 α -graphyne β -graphyne



γ-graphyne



Linear structure ("-C≡C-"),

Free of Cis-trans isomers,

Uniform pores,

Planar polymeric networks,

Highly Conjugated structure.







Graphdiyne : Molecular Structure



Li, Y. Li, Y. et. al., Chem. Soc. Rev. 2014, 43, 2572. Huang, C. Li, Y. et. al., Chin. Sci. Bull. 2016, 61, 2901.

Graphdiyne : Electronic Structure



Graphene, a layer of graphite just one atom thick, isn't called a wonder material for nothing. The subject of the 2010 Nobel Prize in physics, it is famed for its superlative mechanical and electronic properties. Yet new computer simulations suggest that the electronic properties of a little-known sister material of graphene—graphyne—may in some ways be



Promising in the diverse applications

D. Malko et al., Phys. Rev. Lett. 2012, 108, 086804.

A. L. Ivanovskii, Progress in Solid State Chemistry 2013, 41, 1

Synthesis of graphdiyne

Synthetic Route:



Uniform film (1µm), conductivity: 2.516×10^{-4} S/m

Y. L. Li et al., Chem Commun. 2010, 46, 3256

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Graphdiyne nanowalls



- Cu foil (offering Cu⁺ catalyst)
- Ligand: TMEDA or Pyridine
- Hexaethynylbenzene
- 60 °C

N, N, N', N'-tetramethylethylenediamine (TMEDA)



J. Zhou et.al, J. Am. Chem. Soc. 2015, 137, 7596.

QDs-Sensitized GDY Photocathode



hot electrons : 10¹⁰-10¹² s⁻¹

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Hot holes: 10⁸-10⁹ s⁻¹

S. Kundu, A. Patra, Chem. Rev., 2017, 117, 712-757.

Kamat, P. V, Langmuir 2014, 30, 5716-5725.

QDs-Sensitized GDY Photocathode



Li et.al J. Am. Chem. Soc. 2016, 138, 3954.

• Band gap and band position of photoelectrode material must match reaction potentials:



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SC and

Meta

contacts cathode

Metal

anode

Meta.

cathode

ohmic contacts

- Calculations:
 - Photoactive material(s) will show
 diode-like current-potential behavior:
 - Electrochemical system shows losses:
 - Reaction overpotentials
 - Ohmic losses
 - Concentration losses
 - Electrochemical load curve will show electrolyzer like load curve
 - Intersection between both is operating point



$$i = i_L - i_0 \left(\exp\left(\frac{qV}{kT}\right) - 1 \right)$$

 $E = E_0 + \eta_a + \eta_c + iR_{sol} + E_{mem} + E_{conc} > E_0$

Elementary charge

- Calculations:
 - Electrochemical system shows losses:



Ohmic losses account for resistances in electrolyte, membrane, and solid conductor:
 Characteristic ion and electron path length

$$\Delta V_{\rm ohm} = i \rho_{\rm sol} l$$

• Proposed devices



• Proposed devices



US Patent 62/376923 EP Patent 16020308.9







Experimental demonstration



Output power of PEC at 474 kW/m²: 27 W Current density in electrolyzer component: 0.88 A/cm² Current density in photoabsorber component: 6.04 A/cm² Efficiency: 17.1% solar-to-fuel

Photoelectrochemistry - Comparison

• Community outreach: dynamic and online: – <u>http://specdc.epfl.ch/</u>



LEGEND							
Fill color - PV / photoabsorber material	Boundary color - EC material	Symbol shape - PV / photoabsorber and EC configuration					
All III-V	Rare metal-based (expensive)	0	2J, integrated PVs and catalyst	+	3J, integrated PVs and catalyst		
Partial III-V	Abundant (cheap)		2J, integrated PVs, wired catalyst	Δ	3J, integrated PVs, wired catalyst		
All Si			2J, non-integrated PVs or catalyst	0	3J, non-integrated PVs or catalyst		
Partial Si							
Oxides and others							

Tembhurne, Nandjou, Haussener, Nature Energy, doi: 10.1038/s41560-019-0373-7, 2019

Scaling – ongoing @LRESE



kW-scale, long-term, on-sun demonstration, 0.5 kg of hydrogen per day

Scaling – ongoing @LRESE



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Sustainability issue

• Solar to fuels:



Solar materials

- Solar to materials:
 - In principle any other chemical reaction could be driven by solar thermochemistry or photoelectrochemistry if enthalpy of reaction matches solar irradiation, or equilibrium potential and band edge position matches solar irradiation and material combinations

– E.g.:

- Carbothermic reduction of alumina under near vacuum conditions
- Ammonia production



Solar materials

• (Photo)electrochemical:

Absolute Maximum Value per Energy Input vs Minimum Voltage Required



Maximum net value per energy input (log scale) plotted versus minimum voltage required for all electrochemical processes or electrochemical equivalents of thermochemical processes. For each point, the width of the circle corresponds to the relative market size. Processes highlighted in green are conducted electrochemically in industry, to any appreciable extent. The lower bound of feasibility (LBF) is plotted as the horizontal dashed line

Palmer et al., Technoeconomics of Commodity Chemical Production Using Sunlight, ACS Sustainable Chemistry & Engineering, 2018

Learning outcomes of todays lecture

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- Why using fossil fuels together with solar energy?
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- What other chemical commodities or materials can be processed using solar energy?

Solar energy conversion systems

- Literature
 - Review articles:
 - Meier et al., Solar thermochemical production of fuels, Advances in Science and Technology, vol. 74, pp. 303-312, 2010.
 - Lipinski et al., Review of heat transfer research for solar thermochemical applications, Journal of Thermal Science and Engineering Applications, 5: 021005, 2013.
 - Walter et al., Solar water splitting cells, Chemical Reviews, vol. 110, pp. 6446–6473, 2010.